

Article

Influence of Droplet Size on Exergy Destruction in Flow of Concentrated Non-Newtonian Emulsions

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Abstract: The influence of droplet size on exergy destruction rate in flow of highly concentrated oil-in-water emulsions was investigated experimentally in a cone and plate geometry. The oil concentration was fixed at 74.5% by volume. At this dispersed-phase (oil) concentration, two different droplet size emulsions were prepared: fine and coarse emulsions. The fine and coarse emulsions were mixed in different proportions to vary the droplet size distribution. Although the dispersed and matrix phases of the emulsions were Newtonian in nature, the emulsions exhibited a non-Newtonian (shear-thinning) behavior due to the high droplet concentration. The shear stress—shear rate data of the emulsions could be described adequately by a power law model. At low shear rates, the exergy destruction rate per unit volume of emulsion exhibited a minimum at a fine emulsion proportion of 35%. The results from the cone and plate geometry were used to simulate exergy loss in pipeline flow of emulsions. The pumping of emulsions becomes more efficient thermodynamically upon mixing of fine and coarse emulsions provided that the flow regime is maintained to be laminar and that the Reynolds number is kept at a low to moderate value. In the turbulent regime, the exergy loss generally increases upon mixing the fine and coarse emulsions.

Keywords: emulsion; oil-in-water; exergy; entropy; pipeline; flow; droplet size; non-Newtonian; second law

1. Introduction

Emulsions are two-phase dispersions of oil and water [1–3]. One of the phases (oil or water) is dispersed as droplets in a continuum of the other phase. Thus, emulsions could be classified into two broad groups: (i) oil-in-water (abbreviated as O/W) emulsions where oil forms the dispersed droplets and water is the continuous phase; and (ii) water-in-oil (abbreviated as W/O) emulsions where water forms the dispersed droplets and oil is the continuous phase. The applications of emulsions are many. Numerous products of commercial importance are handled or sold in the form of emulsions. The industries where emulsions are frequently encountered in one form or the other include: petroleum, food, pharmaceutical, cosmetics, agriculture, explosives, lubricants, and paints [1,4–13].

The pumping of emulsions through pipelines and other process equipment is a common occurrence in industrial applications. For example, highly viscous heavy crude oils and bitumen are transported over long distances via pipelines in the form of O/W emulsions. As pumping systems consume a significant portion of the total electrical energy used in the process, it is important to quantify the extent to which exergy is destroyed due to irreversibilities in the process. It is equally important from a practical point of view to find ways to minimize the destruction of exergy and hence reduce the pumping costs.

The exergy of a system is defined as the maximum possible useful work that can be obtained from the system when the system is taken from its given state to the dead state where the system is in thermodynamic equilibrium with the environment. A system in thermodynamic equilibrium with its

environment has zero exergy. Thus, exergy is a property that is associated with the state of the system and its environment [14]. The thermo-mechanical exergy of a closed system is given as follows on a unit mass basis:

$$\psi = (u - u_o) + P_o (v - v_o) - T_o (s - s_o) + gz \quad (1)$$

where u , v , and s are specific internal energy, specific volume, and specific entropy of the system, respectively; u_o , v_o , and s_o are specific internal energy, specific volume, and specific entropy of the system in the dead state, respectively; P_o and T_o are the environment pressure and temperature, respectively; g is acceleration due to gravity; and z is the elevation of the system. In Equation (1), it is assumed that the kinetic energy of the system is zero, that is, the system is stationary. The thermo-mechanical exergy associated with a fluid stream per unit mass is given as follows:

$$\psi = (h - h_o) - T_o (s - s_o) + \frac{V^2}{2} + gz \quad (2)$$

where h is the specific enthalpy of the fluid in its current state, h_o is the specific enthalpy of the fluid in the dead state, and V is the velocity of the fluid.

According to the Gouy-Stodola theorem, the amount of exergy destroyed in a process is directly proportional to the total rate of entropy generation in the system and the surroundings, that is:

$$\dot{\Psi}_{destruction} = T_o \dot{S}_{G,total} \quad (3)$$

where $\dot{\Psi}_{destruction}$ is the total rate of exergy destruction, and $\dot{S}_{G,total}$ is the total rate of entropy generation. In the absence of any heat transfer between the system and the surroundings, that is, under adiabatic condition, the external irreversibility is eliminated and therefore, the exergy destruction is entirely due to internal irreversibilities and $\dot{S}_{G,total} = \dot{S}_G$ where \dot{S}_G is the rate of entropy generation within the system or control volume boundary.

In order to improve the thermodynamic efficiency of the process, it is important to estimate the rate of exergy destruction in a process and to minimize it. One possible way to manipulate and control the rate of exergy destruction in emulsion flows is to vary the droplet size distribution. In the past, a number of studies have been published on emulsion rheology [8,9,11,13,15–17] and concurrent flow of oil and water in pipes [18–34]. However, the analysis and interpretation of influence of droplet size and droplet size distribution on exergy destruction in emulsion flows is lacking. In this article, exergy destruction in isothermal flow of emulsions is measured experimentally using a cone and plate geometry. The influence of droplet size distribution on exergy destruction is also determined. To our knowledge, this is the first study on the influence of droplet size distribution on exergy destruction in isothermal flow of emulsions.

2. Theoretical Background

When a fluid is sheared, entropy is generated and exergy is destroyed due to friction in the fluid. Consider a certain volume of incompressible fluid at a uniform temperature T . When this fluid is sheared, work is done on the fluid. Let the rate of work done on the fluid per unit volume basis be \dot{W} . The work supplied to the fluid is dissipated in frictional heating of the fluid. In order to keep the temperature of the fluid uniform at T , let the rate of heat removal from the fluid to its surroundings at T_o be \dot{Q} on a unit volume basis. The exergy balance on the fluid gives:

$$\dot{\psi}_D = \dot{W} - \dot{Q} \left(1 - \frac{T_o}{T} \right) \quad (4)$$

where $\dot{\psi}_D$ is the exergy destruction rate per unit volume of the fluid. Note that both \dot{W} and \dot{Q} are treated as positive quantities as their directions are already specified. From the first law of thermodynamics, $\dot{Q} = \dot{W}$. Thus, Equation (4) reduces to:

$$\dot{\psi}_D = \dot{Q} \left(\frac{T_o}{T} \right) \tag{5}$$

The rate of energy dissipation in frictional heating of the fluid per unit volume of fluid is given as $\underline{\tau} : \nabla \vec{V}$, where $\underline{\tau}$ is the viscous stress tensor, \vec{V} is the fluid velocity vector, “:” is the double dot product sign [35]. As \dot{Q} is equal to $\underline{\tau} : \nabla \vec{V}$, Equation (5) gives:

$$\dot{\psi}_D = \frac{T_o}{T} \left(\underline{\tau} : \nabla \vec{V} \right) \tag{6}$$

The entropy balance on the fluid gives:

$$\dot{S}_G^v = \left(\frac{\dot{Q}}{T} \right) \tag{7}$$

where \dot{S}_G^v is the rate of entropy generation in the fluid on a unit volume basis. From Equations (5) to (7) it follows that:

$$\dot{\psi}_D = T_o \dot{S}_G^v = \frac{T_o}{T} \left(\underline{\tau} : \nabla \vec{V} \right) \tag{8}$$

In this work, the exergy destruction experiments are carried out in a cone-and-plate rheometer. A cone and plate rheometer is widely used to measure the viscosity and rheology of fluids. It consists of a flat circular plate which is held stationary. A cone rotates at the top of the plate with a known angular velocity. The apex of the cone just touches the bottom plate. The test liquid is placed in the narrow gap between the cone and plate. The angle between the cone and the plate is typically less than 5° (see Figure 1).

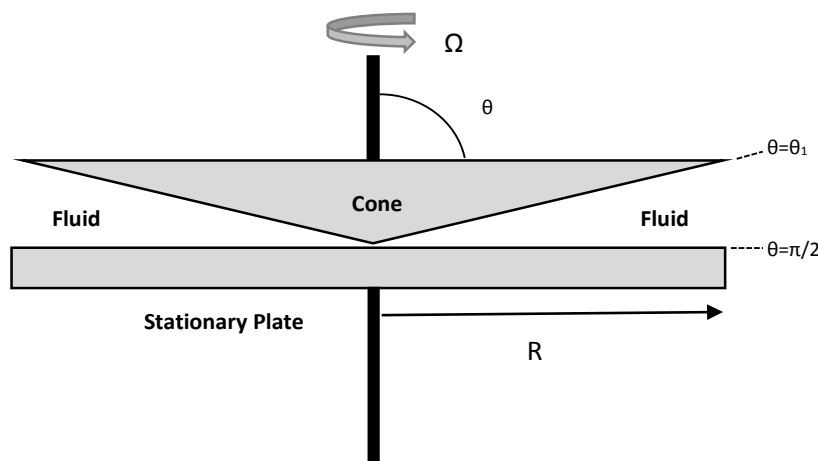


Figure 1. Schematic diagram of a cone-and-plate viscometer.

Exergy Destruction in a Cone-and-Plate Viscometer

The velocity distribution in a cone and plate viscometer is given as [36,37]:

$$V_\phi = \Omega r \sin \theta_1 \left[\frac{\cot \theta + \frac{\sin \theta}{2} \ln \left(\frac{1 + \cos \theta}{1 - \cos \theta} \right)}{\cot \theta_1 + \frac{\sin \theta_1}{2} \ln \left(\frac{1 + \cos \theta_1}{1 - \cos \theta_1} \right)} \right] \tag{9}$$

As the motion is in ϕ -direction, only V_ϕ is non-zero. The other two components of velocity (V_r and V_θ) are zero. Since $\theta_1 \approx \frac{\pi}{2}$ and $\theta \approx \frac{\pi}{2}$, this expression of velocity simplifies to $V_\phi = \Omega r \cos \theta / \cos \theta_1$.

Using the velocity distribution and the symmetry of stress tensor, it can be readily shown that [36,37]:

$$\underline{\underline{\tau}} : \nabla \vec{V} = - \left(\frac{\tau_{\theta\varphi}\Omega}{\cos\theta_1} \right) \left(\frac{1}{\sin\theta} \right) \approx - \left(\frac{\tau_{\theta\varphi}\Omega}{\cos\theta_1} \right) \quad (10)$$

Note that $\theta \approx \frac{\pi}{2}$ in a cone-and-plate viscometer. The shear rate in the cone-and-plate viscometer $\dot{\gamma}$ is given as [35]:

$$\dot{\gamma} = \left(\frac{\Omega}{\cos\theta_1} \right) \left(\frac{1}{\sin\theta} \right) \approx \left(\frac{\Omega}{\cos\theta_1} \right) \quad (11)$$

Combining Equations (10) and (11), we get:

$$\underline{\underline{\tau}} : \nabla \vec{V} = (-\tau_{\theta\varphi}) \dot{\gamma} \quad (12)$$

where $\dot{\gamma}$ and $-\tau_{\theta\varphi}$ are positive quantities.

The local exergy destruction rate per unit volume of the fluid given by Equation (8) can now be expressed for a cone-and-plate viscometer as:

$$\dot{\psi}_D = T_o \dot{S}_G = \frac{T_o}{T} \left(\underline{\underline{\tau}} : \nabla \vec{V} \right) = \frac{T_o}{T} (\tau \dot{\gamma}) \quad (13)$$

where $\tau (= -\tau_{\theta\varphi})$ is the shear stress measured through the torque transmitted to the bottom stationary plate and $\dot{\gamma}$ is the shear rate in the viscometer determined from the angular speed of rotation of the cone (see Equation (11)). It is important to note that the shear rate $\dot{\gamma}$ in a cone-and-plane viscometer is uniform in that it does not vary with the position in the flow field (space in between the rotating cone and stationary plate).

3. Experimental Section

The emulsions prepared were of O/W type, that is, oil droplets formed the dispersed-phase and water formed the continuous phase. The oil used was a petroleum oil of viscosity 5.8 mPa·s at 25 °C. The water used was deionized. A water-soluble non-ionic surfactant Triton X-100 was used to stabilize the emulsions. The concentration of the surfactant was kept 2 wt % based on the aqueous phase. The emulsions were prepared in batches of about 500 g using a variable speed homogenizer to provide the necessary shearing. The oil concentration (ϕ) was fixed at 74.5% by volume. At this dispersed-phase (oil) concentration, two different droplet size emulsions were prepared: fine and coarse emulsions. For the preparation of coarse emulsion, the shearing speed of the homogenizer was kept low and the emulsion was sheared for a small duration. A high shearing speed and increased duration of shearing were used for the preparation of fine emulsion. The fine and coarse emulsions produced were highly stable in nature. Several mixtures of fine and coarse emulsions were also prepared by mixing them in varying proportions using gentle stirring with a hand stirrer. The rheological and exergy destruction behaviors of the fine and coarse emulsions as well as their mixtures were studied at a fixed temperature of 25 °C using a controlled-stress rheometer with a cone-and-plate geometry. The plate was kept stationary and the cone was rotated at different angular speeds. The cone diameter was 40 mm and the plate diameter was 60 mm. The angle between the cone surface and stationary plate was 4° and the gap at the cone tip was 150 μm. The droplet sizes of emulsions were determined by taking photomicrographs with a Zeiss optical microscope equipped with a camera.

4. Results and Discussion

4.1. Droplet Size Distribution of Emulsions

The photomicrographs of fine and coarse O/W emulsions are shown in Figure 2. The comparison of the droplet size distributions of fine and coarse O/W emulsions is given in Figure 3. The fine emulsion is relatively more uniform in droplet size as compared with the coarse emulsion. The Sauter

mean diameters of the fine and coarse emulsions are 6.3 and 20 μm , respectively. Thus, the coarse emulsion droplets are more than 3 times larger in size than the fine emulsion droplets.

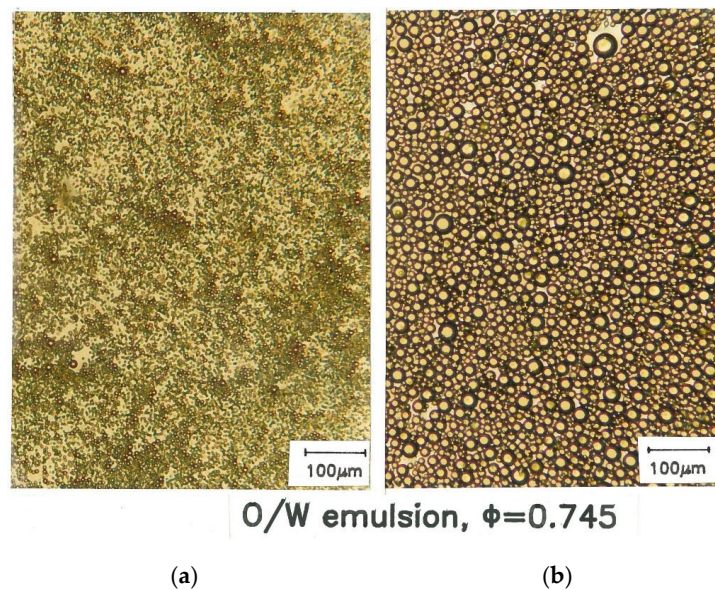


Figure 2. Photomicrographs of fine (a) and coarse (b) O/W emulsions.

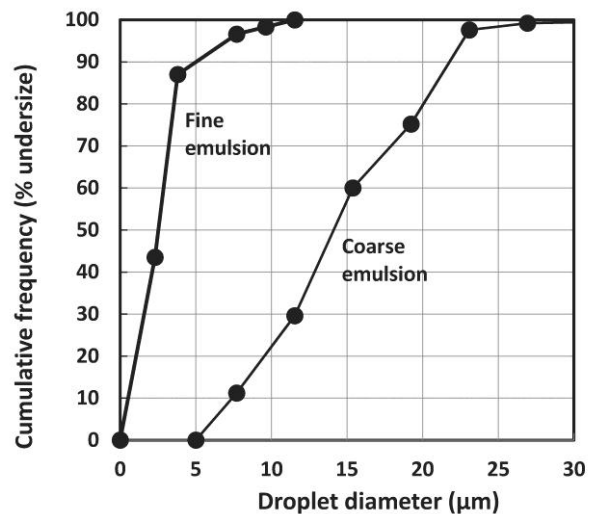


Figure 3. Comparison of droplet size distributions of fine and coarse O/W emulsions.

4.2. Rheology of Emulsions

Figure 4 shows the shear stress *versus* shear rate plots for fine and coarse emulsions and their mixtures, at a fixed ϕ (volume fraction of oil) of 0.745. The plots are almost linear on a log-log scale indicating that emulsions follow the power-law behavior:

$$\tau = K\dot{\gamma}^n \quad (14)$$

where K and n are power-law constants. The slope of the plot, that is, n value, is 0.36 for the fine emulsion and 0.44 for the coarse emulsion. Thus, the coarse emulsion is less non-Newtonian or shear-thinning as compared with the fine emulsion. Table 1 summarizes the statistical information regarding the power-law fit of shear stress *versus* shear rate data for emulsions. Based on the

information given in Table 1, it is clear that the power-law model is generally a reasonably good model to describe the shear stress—shear rate data of the emulsions shown in Figure 4. The only exception is the fine emulsion as in this case the power-law fits the data somewhat approximately.

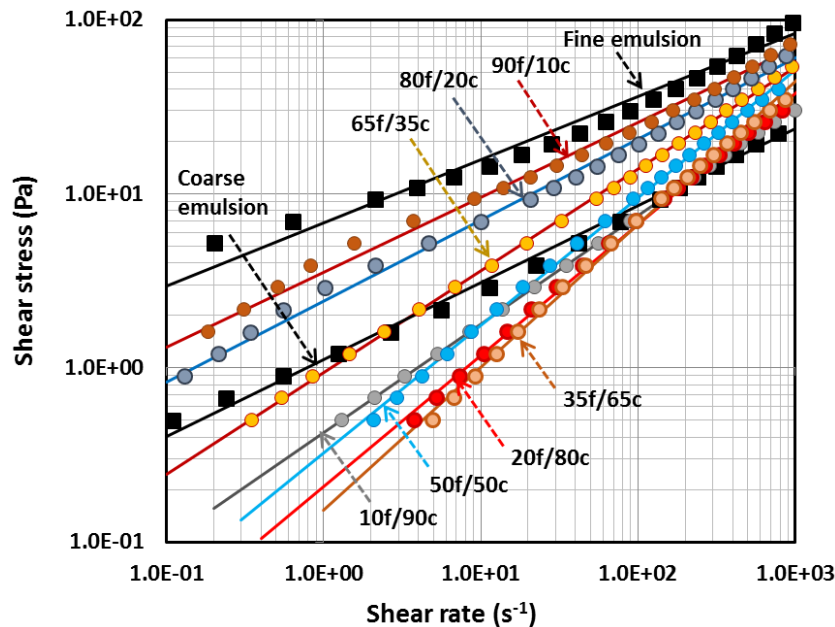


Figure 4. Shear stress *versus* shear rate plots for mixtures of fine and coarse O/W emulsions. In the figure “f” refers to proportion of fine emulsion and “c” refers to proportion of coarse emulsion.

Table 1. Goodness of fit of power-law model and confidence intervals for the power-law parameters.

Emulsion Composition	Regression Correlation Coefficient, R^2	Flow Behavior Index, n	Consistency Index, K (Units of $\text{Pa} \cdot \text{s}^n$)	95% Confidence Interval of n	95% Confidence Interval of K
Coarse (0f/100c)	0.9956	0.442	1.12	[0.427, 0.456]	[1.044, 1.199]
10f/90c	0.9999	0.622	0.425	[0.619, 0.625]	[0.420, 0.430]
20f/80c	0.9975	0.753	0.208	[0.734, 0.771]	[0.191, 0.227]
35f/65c	0.9976	0.822	0.152	[0.802, 0.841]	[0.138, 0.167]
50f/50c	0.9989	0.733	0.323	[0.722, 0.744]	[0.307, 0.340]
65f/35c	0.9996	0.585	0.937	[0.580, 0.591]	[0.916, 0.959]
80f/20c	0.9966	0.466	2.418	[0.454, 0.478]	[2.303, 2.539]
90f/10c	0.9973	0.431	3.522	[0.422, 0.441]	[3.383, 3.667]
Fine (100f/0c)	0.9745	0.364	6.777	[0.336, 0.392]	[5.927, 7.749]

An important point to note from Figure 4 is that the shear stress at any given shear rate is much higher for the fine emulsion indicating that the fine emulsion is much more viscous than the coarse emulsion. When the fine and coarse emulsions are mixed by adding fine emulsion progressively to the coarse emulsion, the slope of the shear stress *versus* shear rate increases initially with the increase in fine emulsion proportion of the mixed emulsion. For example, the n -value increases from 0.44 to 0.82 when the fine emulsion proportion of the mixed emulsion is increased from 0% to 35%. With further increase in fine emulsion content of the mixed emulsion, n decreases. The plots of power-law parameters (K and n) as functions of fine emulsion proportion of the mixed emulsion are shown in Figure 5. The power-law index “ n ” exhibits a maximum whereas the consistency index “ K ” exhibits a minimum at a fine emulsion proportion of 35%.

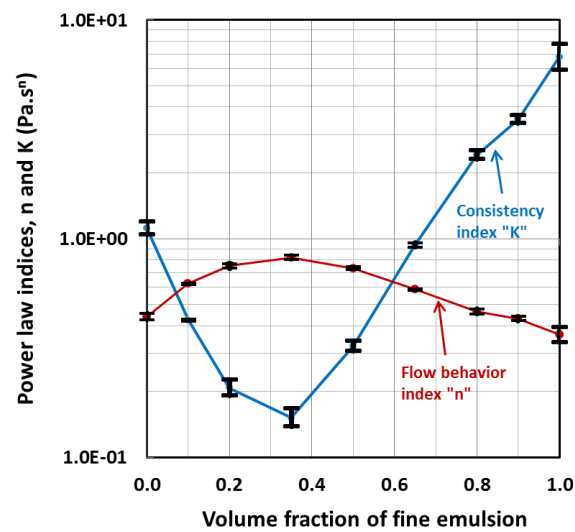


Figure 5. Power law parameters (K and n) with error bars for mixtures of fine and coarse O/W emulsions.

4.3. Reliability of Rheological Measurements

To check the reliability of the rheological measurements carried out in a cone and plate viscometer, some measurements were carried out in a co-axial cylinder viscometer as well. The same emulsion was tested in a cone-and-plate and co-axial cylinder viscometer. Figure 6 compares the rheological data obtained for the fine and coarse emulsions using different instruments. The data obtained from coaxial cylinder viscometer using two different gap-widths almost overlaps with the data obtained from the cone-and-plate viscometer. Thus, the rheological data obtained from the cone-and-plate viscometer are reliable.

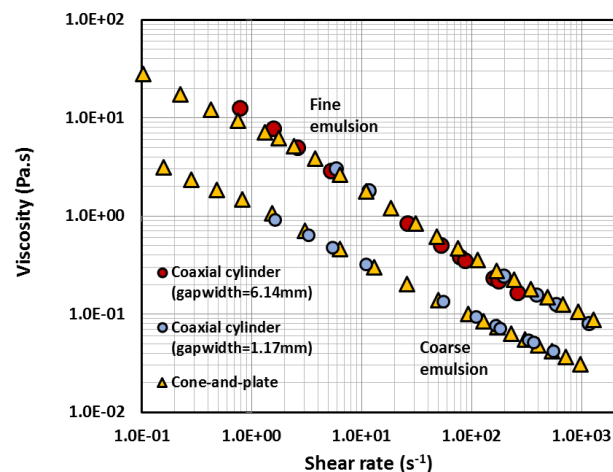


Figure 6. Comparison of viscosity data of fine and coarse emulsions obtained from different instruments.

4.4. Exergy Destruction in Emulsions

The exergy destruction rate per unit volume of the emulsion, that is, ψ_D , is calculated from shear stress-shear rate data using Equation (13). In the present work, the surroundings temperature is taken to be 25 °C, that is, $T = T_0 = 298.15$ K. Figure 7 shows the plots of exergy destruction rate per unit volume of emulsion (ψ_D) as functions of shear stress. For any given shear stress, the exergy destruction

rate is the lowest in fine emulsion. The exergy destruction rate is much higher in the case of coarse emulsion. This appears to be counter-intuitive as fine emulsion is much more viscous and energy dissipative in comparison with the coarse emulsion. The main reason for this apparent contradiction is that the shear rate in coarse emulsion is much higher than that in the fine emulsion when comparison is made at the same shear stress. Therefore it is more appropriate to compare exergy destruction rates in different emulsions at the same shear rate (instead of the same shear stress). To that end, the data of Figure 7 are re-plotted in Figure 8 as $\dot{\psi}_D$ versus shear rate. Now the exergy destruction rate in fine emulsion is the highest as expected.

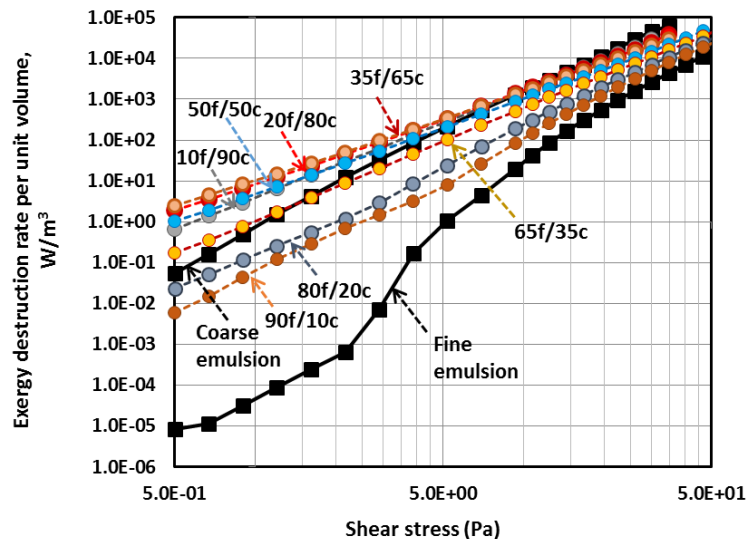


Figure 7. Exergy destruction rate versus shear stress for mixtures of fine and coarse O/W emulsions.

In terms of pumping of emulsion through a pipeline, it can be stated that for the same pressure drop (that is, same shear stress), the flow rate of coarse emulsion will be much higher than that of the fine emulsion. As exergy destruction rate represents the product of pressure drop and flow rate, the exergy destruction rate is therefore expected to be much higher in the case of the coarse emulsion as exhibited in Figure 7. When the comparison is made at the same flow rate (that is, same shear rate), the fine emulsion is expected to give a much higher pressure drop, and hence a much higher rate of exergy destruction, as compared with the coarse emulsion as indicated in Figure 8.

Figure 9 shows the plots of shear rate and exergy destruction rate for mixed fine and coarse emulsions at a fixed shear stress of 0.5 Pa. Both shear rate and exergy destruction rate reach a maximum value at a fine emulsion proportion of about 35%. It should be noted that the shear rate and exergy destruction rate in coarse emulsion are higher than the corresponding values for the fine emulsion at a given stress (0.5 Pa), as pointed out earlier. However, when comparison is made at the same shear rate as shown in Figure 10, the exergy destruction rate in fine emulsion is higher than that in the coarse emulsion. Furthermore, a minimum (instead of maximum) in exergy destruction rate is observed at a fine emulsion proportion of about 35% when comparison is made at the same shear rate.

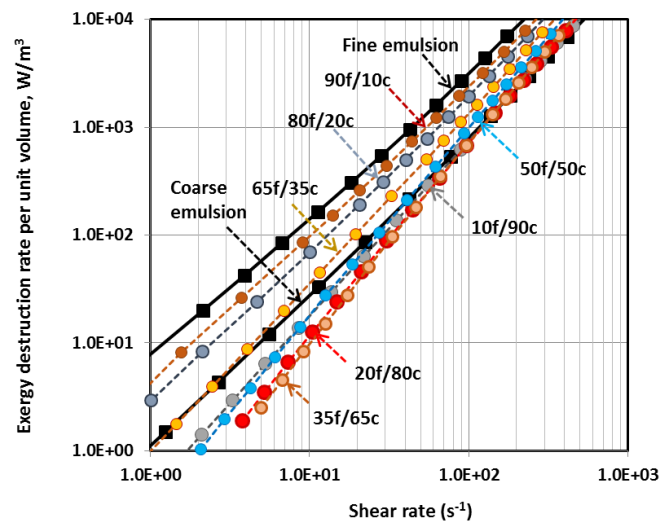


Figure 8. Exergy destruction rate *versus* shear rate for mixtures of fine and coarse O/W emulsions.

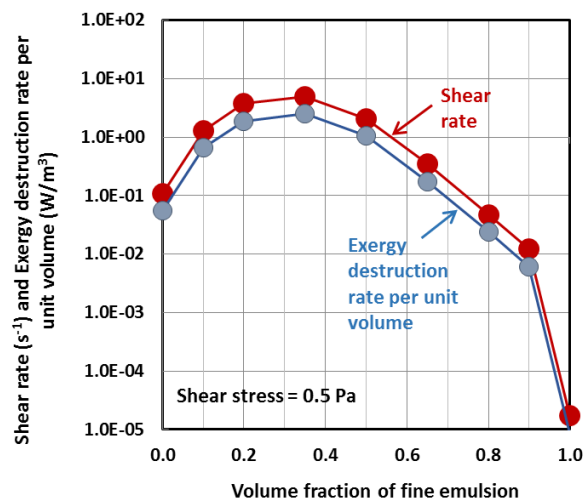


Figure 9. Shear rate and exergy destruction rate for mixtures of fine and coarse O/W emulsions at a fixed shear stress of 0.5 Pa.

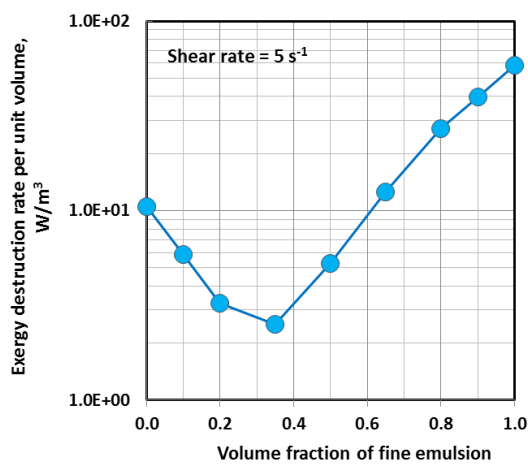


Figure 10. Exergy destruction rate per unit volume for mixtures of fine and coarse O/W emulsions at a fixed shear rate of 5 s^{-1} .

5. Simulation of Exergy Destruction in Pipeline Flow of Emulsions

One important application of this study is in the pipeline transportation of emulsions. Thus, it is important to simulate the influence of droplet size distribution on exergy destruction rate in pipeline flow of emulsions. In a recent study, Pal [38] has proposed the following expressions for entropy production in adiabatic and nearly isothermal pipeline flow of non-Newtonian power-law fluids:

$$\dot{S}'_G = \left(\frac{8\pi}{T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] (\text{Re}_n)^{(1+n)/(2-n)} \quad \text{laminar flow} \quad (15)$$

$$\dot{S}'_G = \left(\frac{\pi}{2T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] \alpha_n (\text{Re}_n)^{(3/(2-n))-\beta_n} \quad \text{turbulent flow} \quad (16)$$

where \dot{S}'_G is the rate of entropy production per unit length of pipe, Re_n is the generalized Reynolds number, D is the pipe diameter, T is the fluid temperature, ρ is the fluid density, and a_n , α_n , β_n are given as follows:

$$a_n = K8^{n-1} \left[\frac{3n+1}{4n} \right]^n \quad (17)$$

$$\alpha_n = 0.0077 \ln(n) + 0.078 \quad (18)$$

$$\beta_n = 0.25(n)^{-0.22} \quad (19)$$

Note that the generalized Reynolds number for power-law fluids is defined as:

$$\text{Re}_n = \frac{\rho D^n \bar{V}^{2-n}}{K8^{n-1} \left[\frac{3n+1}{4n} \right]^n} \quad (20)$$

where K and n are power-law constants, defined in Equation (14).

Using the Gouy-Stodola theorem, Equation (3), the entropy production equations, Equations (15) and (16), could be re-cast in terms of exergy destruction rate per unit length of pipe as:

$$\dot{\psi}'_D = 8\pi \left(\frac{T_o}{T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] (\text{Re}_n)^{(1+n)/(2-n)} \quad \text{laminar flow} \quad (21)$$

$$\dot{\psi}'_D = \frac{\pi}{2} \left(\frac{T_o}{T} \right) \left[\frac{(a_n)^{3/(2-n)}}{\rho^{(1+n)/(2-n)} D^{(4n-2)/(2-n)}} \right] \alpha_n (\text{Re}_n)^{(3/(2-n))-\beta_n} \quad \text{turbulent flow} \quad (22)$$

where $\dot{\psi}'_D$ is the exergy destruction rate per unit pipe length in adiabatic pipeline flow of non-Newtonian power-law fluids and T_o is the surroundings temperature. Equations (21) and (22) are used to simulate the influence of droplet size on $\dot{\psi}'_D$ in adiabatic pipeline flow of power-law O/W emulsions. The influence of droplet size on $\dot{\psi}'_D$ enters the analysis through the power-law parameters K and n , which are dependent on the droplet size distribution of emulsion (see Figure 5).

Figure 11 shows the exergy destruction plots for adiabatic laminar flow of mixtures of fine and coarse O/W emulsions in a pipeline of diameter 26.54 mm. The plots are generated using Equation (21) and the power law constants for mixtures of fine and coarse emulsions shown in Figure 5.

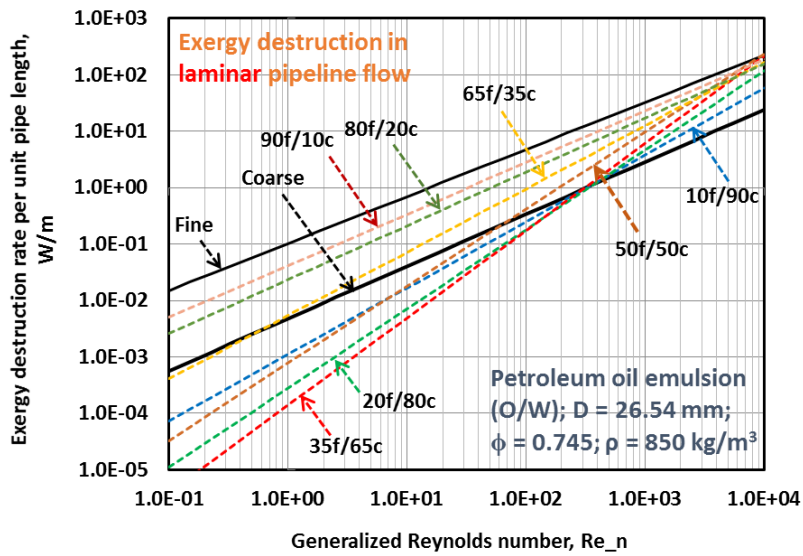


Figure 11. Exergy destruction rate per unit pipe length in adiabatic laminar flow of mixtures of fine and coarse O/W emulsions.

The exergy destruction rate in fine emulsion is substantially higher than that in the coarse emulsion over the full range of Re_n . Upon mixing the fine emulsion with the coarse emulsion in moderate amounts (fine emulsion proportion less than 50%), the exergy destruction rate falls well below that of the coarse emulsion at low to moderate values of the generalized Reynolds number Re_n . When fine emulsion proportion of the mixed emulsion is larger than 50%, the exergy destruction rates fall in between those of the coarse and fine emulsions. At high values of Re_n , the exergy loss rates for mixed emulsions always fall in between those of the coarse and fine emulsions, regardless of the proportion of the fine emulsion. Figure 12 clearly shows the effect of Re_n on exergy loss in mixed emulsions. At a low Re_n value of 0.1, the exergy destruction rate exhibits a minimum at a fine emulsion proportion of about 35%. However, at a high Re_n value of 1122 the exergy destruction rate increases linearly with the fine emulsion content of the mixed emulsion. Thus, it can be concluded that the influence of droplet size distribution in improving the thermodynamic efficiency of pumping of emulsions is restricted to modest values of Re_n .

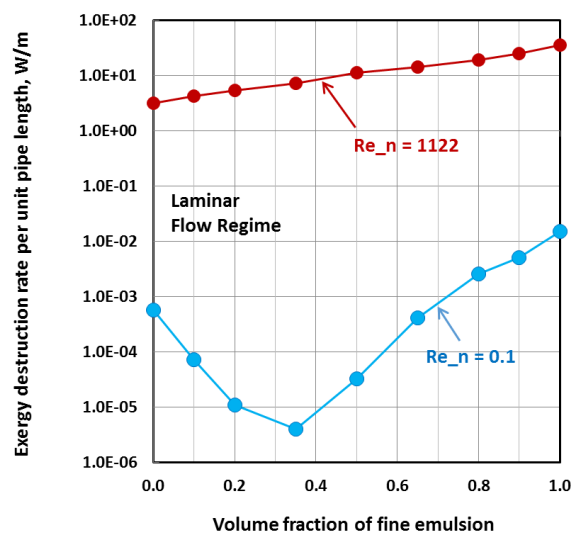


Figure 12. The effect of Re_n on exergy loss in adiabatic pipeline flow of mixtures of fine and coarse O/W emulsions.

The mitigation of exergy loss in pipeline flow of mixtures of fine and coarse emulsions at high dispersed-phase concentration ($\phi = 0.745$ in the present study) is due to the fact that fine droplets can easily fit into the voids created by close packing of large droplets. As a result, the mixed emulsion of small and large droplets is less densely packed and hence less dissipative in nature as compared with an emulsion of uniform size droplets.

Figure 13 shows the exergy destruction plots for adiabatic turbulent flow of mixtures of fine and coarse O/W emulsions in a pipeline of diameter 26.54 mm. The plots are generated using Equation (22) and the power law constants for mixtures of fine and coarse emulsions shown in Figure 5. The exergy destruction rate in fine emulsion is substantially higher than that in the coarse emulsion over the full range of Re_n , as expected due to more dissipative nature of the fine emulsion. However, upon mixing the fine emulsion with the coarse emulsion, the exergy destruction rates generally fall above those of the coarse and fine emulsions. This can be seen more clearly in Figure 14. Interestingly, the exergy destruction rate in mixed emulsions also exhibits a maximum at a fine emulsion proportion of about 35%.

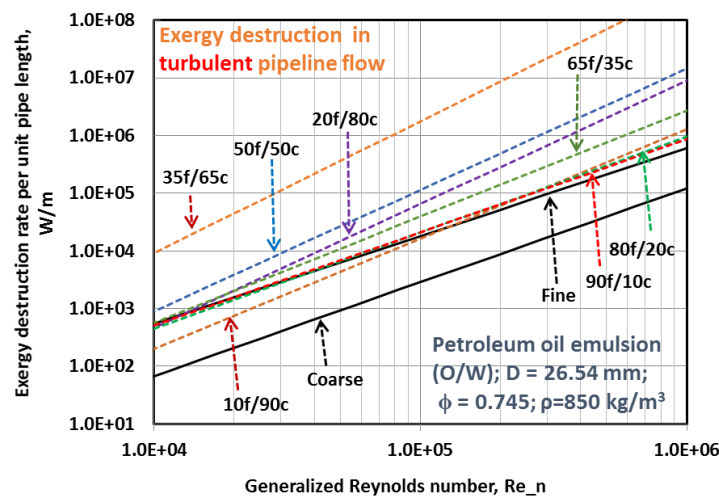


Figure 13. Exergy destruction rate per unit pipe length in adiabatic turbulent flow of mixtures of fine and coarse O/W emulsions.

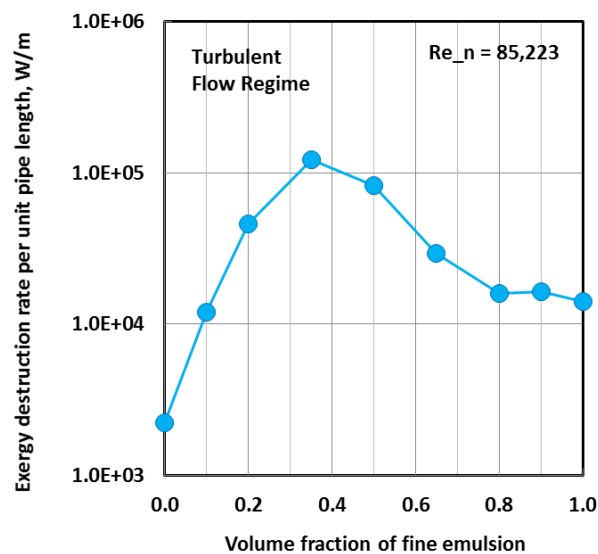


Figure 14. Exergy destruction rate in adiabatic turbulent flow of mixtures of fine and coarse O/W emulsions at a fixed Re_n of 85,223.

According to Equation (22), the plot of exergy destruction rate $\dot{\psi}'_D$ versus Reynolds number Re_n is dependent on the power-law parameters K and n . With the increase in K , the emulsion becomes more dissipative in nature and therefore the plot shifts upward reflecting an increase in exergy loss. With the increase in the power law index n , and hence a decrease in the degree of pseudo-plasticity of emulsion, the slope of $\dot{\psi}'_D$ versus Re_n increases indicating a larger increase in exergy loss with the increase in Reynolds number. When fine emulsion is mixed with a coarse emulsion, the power law index n increases as shown in Figure 5. The power-law index also exhibits a maximum at a fine emulsion proportion of about 35%. Thus, the increase in the exergy destruction rate when fine and coarse emulsions are mixed, as observed in Figures 13 and 14 is dominated by an increase in n .

6. Conclusions

Based on the analysis and experimental work presented in this article, the following conclusions can be made:

- The shear-stress τ versus shear rate $\dot{\gamma}$ behavior of concentrated oil-in-water emulsions (fine, coarse, and their mixtures) investigated in this work can be described satisfactorily by a power-law model $\tau = K\dot{\gamma}^n$. The power-law parameters K and n vary with the droplet size and droplet size distribution of emulsions. When fine emulsion (small droplet size) is mixed with the coarse emulsion (large droplet size), keeping the dispersed-phase concentration fixed, the consistency index K goes through a minimum and the power-law index n goes through a maximum at a certain proportion of fine emulsion content of the mixed fine and coarse emulsion.
- The exergy destruction rate per unit volume of emulsion exhibits a minimum when fine emulsion is mixed with the coarse emulsion. The minimum in exergy destruction rate is observed at low shear rates around the fine emulsion proportion of 35%.
- The thermodynamic efficiency of pumping emulsion through a pipeline increases when fine emulsion is mixed with the coarse emulsion provided that the flow regime is laminar and that the Reynolds number is not high (less than about 100).
- At high Reynolds number in the turbulent regime, the exergy loss in pipeline flow of emulsion increases upon mixing fine emulsion with the coarse emulsion, keeping the dispersed-phase concentration fixed. The increase in exergy loss upon increasing the droplet size distribution is due an increase in the flow behavior index n (a decrease in pseudo-plasticity).

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