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Authors:

Minghao Chen, Zuhua Xu, Jun Zhao

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Article

Triple-Mode Model Predictive Control Using Future Target Information

Minghao Chen, Zuhua Xu and Jun Zhao *

National Center for International Research on Quality-Targeted Process Optimization and Control, College of Control Science and Engineering, Zhejiang University, Hangzhou 310027, China; mh_chen@zju.edu.cn (M.C.); zhxu@zju.edu.cn (Z.X.)

* Correspondence: jzhao@zju.edu.cn

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Abstract: In this paper, we propose a triple-mode model predictive control (MPC) algorithm that uses future target information to improve tracking performance. To explicitly take into account the future target information in the MPC optimization, the proposed triple-mode control law encompasses three parts: (i) the future target information feedforward, (ii) the output feedback, and (iii) the extra degrees of freedom for constraint satisfaction. The first two parts of the control law are off-line designed through unconstrained MPC, and the optimal future trajectory horizon is obtained by golden section search based on the integral of squared error (ISE) criterion. The final part is calculated by the on-line MPC algorithm aiming to satisfy constraints. Furthermore, we analyze the feasibility and convergence properties of the proposed algorithm. The method is demonstrated by the simulation of the shell fundamental control problem and also tested on the coordinated control problem in the power plant. The test results show that the proposed algorithm can increase tracking performance dramatically due to the proper selection of future trajectory horizon.

Keywords: model predictive control; dynamic matrix control; future target information; future trajectory horizon

1. Introduction

Concern about multivariable constrained system control has become a central issue in the control domain. As a result, much research in recent years has focused on the development of advanced control algorithms that are process friendly. Model predictive control (MPC) has been widely and successfully applied in the process industry, primarily due to its superior performance and the capability of dealing with a multivariate constrained problem [1–3]. Since the step-response model is more convenient to obtain and more suitable for the process industry, this model has been successfully applied to numerous industrial processes by Aspen Technology, Honeywell Hi-Spec, and others. There has been an increase in the adoption of dynamic matrix control in MPC commercial software packages such as DMC+, SMC, RMPCT, HIECON [1].

The key idea of model predictive control is to use the historical information and model prediction to calculate the optimal input trajectory by minimizing the deviation between the process output and the desired target in a receding horizon way. There exists a rich supporting theory [4–6] for its success in industry. Moreover, the applications of model predictive control have already gone beyond petrochemical or chemical industries and extended to power plants [7], traffic, robots [8] and any other fields.

The research to date has tended to focus on the regulation problem (steer the system to the origin) [4] for facilitating the analysis and design. The regulation problem assumes the hypothesis that the future setpoint is fixed or changes instantaneously, thus future target information is rarely discussed

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in the current literature. Considering the setpoint changes, Limón et al. [9] adopted a modified cost function and a stabilizing extended terminal constraint in MPC optimization to obtain the feasible setpoints in case that the setpoints are not feasible. Their work is still preserving no consideration of using the future target information. The MPC optimization have the capability of considering the future target information [10], which may be helpful in control since it allows the controller to react to the setpoint changes in advance [11]. Carrasco and Goodwin [12] proposed a feedforward model predictive control, in which the feedforward was designed individually before the feedback design. However, how much future target information (so-called "preview" in their work) should be used in feedforward design is not discussed in their work. Rossiter and Grinnell [13] developed an extended input horizon generalized predictive controller (EIHGPC) algorithm, in which they parameterized the degrees of freedom to spread the control increments over the prediction horizon and adopted a heuristic algorithm to select a proper future target horizon, hence improves the tracking performance. Their method only pertains to the unconstrained case. In [14], the authors proposed a dual-mode constrained MPC algorithm, which was composed of a linear state feedback and extra degrees of freedom. Under such a control law, the feedforward could not be designed individually and the future target horizon was determined through a trial and error process.

However, the inappropriate use of future target information may cause the deterioration of control performance [13,15]. There remains a need for an effective method that can determine a proper future target horizon. Moreover, the current implementations of MPC fail to separately design the feedforward, feedback and constraint satisfaction, which could not yield the desirable performance from each part. In this study, a triple-mode constrained model predictive control algorithm is developed, which has the merit of independent design for each mode of the control law. The main ingredients of the triple-mode control law are: (i) the feedforward design using future target information, (ii) the output feedback, and (iii) the extra degrees of freedom for constraint satisfaction. In addition, a golden section search method is proposed to optimize the future trajectory horizon, which can be used to design the feedforward to improve the tracking performance.

The outline of this article is as follows. First, we describe the typical dynamic matrix control. Next, we give the future target information feedforward structure derived from the unconstrained control law and propose an optimization method for the selection of future trajectory horizon. We then introduce the triple-mode model predictive control using future target information. Finally, we provide two illustrative simulation examples.

2. Preliminary

Mathematical notations used throughout this paper are defined as follows. Given a vector $x \in \mathbb{R}^n$, the symbol ||x|| denotes the Euclidean 2-norm and $||x||_P^2$ denotes the quadratic form of x. e.g., $||x||_P^2 = x^T P x$; A^T denotes the transpose of A; Given two integers, $l \le m$, we define the set $\mathbb{I}_{l:m} = \{l, l+1, ..., m-1, m\}$. The superscript * denotes the optimal solution or cost according to the context.

Dynamic Matrix Control Algorithm

The design of the MPC algorithm in this paper follows the standard DMC approach proposed by Garcia and Morshedi [2]. Without loss of generality, we consider a MIMO linear dynamic system with $n_y \in \mathbb{R}$ controlled variables and $n_u \in \mathbb{R}$ manipulated variables. The DMC algorithm adopts a non-parametric step response model as the predictor, thus the ith output $y_i(t) \in \mathbb{R}$ at time t can be formulated by the following step response model

$$y_i(t) = \sum_{j=1}^{n_u} \sum_{k=1}^{\infty} a_{i,j,k} \Delta u_j(t-k), (1 \le j \le n_y)$$
 (1)

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in which $\Delta u_j(t) \in \mathbb{R}$ denotes the jth input increment, i.e., $\Delta u_j(t) := u_j(t) - u_j(t-1)$. $a_{i,j,k} \in \mathbb{R}$ denotes the kth element of the corresponding step response, and the step response sequence of the ith output to the jth input is $\{a_{i,j,1}, a_{i,j,2}, ..., a_{i,j,n}, ...\}$. For a stable plant this sequence will asymptotically reach a constant value, i.e., $a_{i,j,n+m} \approx a_{i,j,n}$ (m > 0).

Based on the step response model, the output predictions over n future steps can be expressed as follows

$$Y(t+1) = \Lambda Y(t) + A\Delta u(t)$$
 (2)

where

$$Y(t) = [y^{T}(t|t-1), y^{T}(t+1|t-1), ..., y^{T}(t+n-1|t-1)]^{T}$$

$$y(t+k|t-1) = [y_{1}(t+k|t-1), y_{2}(t+k|t-1), ..., y_{n_{y}}(t+k|t-1)]^{T}, \forall k \in \mathbb{I}_{0:n-1}$$

$$\Delta u(t) = [\Delta u_{1}(t), \Delta u_{2}(t), ..., \Delta u_{n_{u}}(t)]^{T}$$

$$A = \begin{bmatrix} 0 & I_{n_{y}} & 0 & \cdots & 0 & 0 \\ 0 & 0 & I_{n_{y}} & \cdots & 0 & 0 \\ \vdots & \vdots & \vdots & \ddots & \vdots & \vdots \\ 0 & 0 & 0 & \cdots & I_{n_{y}} & 0 \\ 0 & 0 & 0 & \cdots & 0 & I_{n_{y}} \end{bmatrix}, A = \begin{bmatrix} A_{1} \\ A_{2} \\ \vdots \\ A_{n} \end{bmatrix}$$

$$A_{t} = \begin{bmatrix} a_{1,1,t} & a_{1,2,t} & \cdots & a_{1,n_{u},t} \\ a_{2,1,t} & a_{2,2,t} & \cdots & a_{2,n_{u},t} \\ \vdots & \vdots & \ddots & \vdots \\ a_{n-1}t & a_{n-2}t & \cdots & a_{n-n}t \end{bmatrix}, \forall t \in \mathbb{I}_{1:n}$$

 $\Delta u(t) \in \mathbb{R}^{n_u}$ is a vector of the future control moves at time t. $Y(t) \in \mathbb{R}^{n_y \cdot n}$ is the dynamic states of the system, and $y(t+k|t-1) \in \mathbb{R}^{n_y}$ is the future output vector at time t+k assuming the input remain constant starting at time t-1, which means $\Delta u(t+j) = \mathbf{0}$ for $j \geq 0$. The evolution of predictions can be obtained by translation of one-step prediction plus the contribution made by the latest control move $\Delta u(t)$.

To achieve the goal of offset-free tracking, a bias is introduced into the model to incorporate the feedback. It's assumed that the model prediction and the measured output at the current time is due to a constant step disturbance at the output. The constant output step disturbance assumption is standard in industrial applications [16]. The model bias $e(t) \in \mathbb{R}^{n_y}$ is based on the latest output measurement $\hat{y}(t) \in \mathbb{R}^{n_y}$ and the predicted outputs $\hat{y}(t|t-1) \in \mathbb{R}^{n_y}$

$$e(t) = \tilde{\mathbf{y}}(t) - \hat{\mathbf{y}}(t|t-1) \tag{3}$$

in which $\hat{y}(t|t-1)$ refers to the prediction of output at time t based on the measurements up to time t-1. The bias is added to compensate the output prediction

$$\hat{\mathbf{Y}}(t|t) = \hat{\mathbf{Y}}(t|t-1) + He(t) \tag{4}$$

where $\hat{Y}(t|t-1)$ denotes the estimate of Y(t) at time t before the latest measurements are obtained. $\hat{Y}(t|t)$ is the revised estimate of Y(t) on the basis of the feedback, and $H := diag\{I_{n_y}, ..., I_{n_y}\}$ refers to the weighting matrix of the bias term.

For open-loop stable systems, the future control moves $\Delta U_M(t) \in \mathbb{R}^{M \cdot n_u}$ over the control horizon (M) is optimized to drive the model predicted outputs $\hat{Y}_P(t+1|t) \in \mathbb{R}^{P \cdot n_y}$ as closely as possible to

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a desired future trajectory $R(t+1|t) \in \mathbb{R}^{P \cdot n_y}$ over prediction horizon (P). The DMC optimization problem is defined as

$$\min_{\Delta u_M(t)} J(t) = \|R(t+1|t) - \hat{\mathbf{Y}}_P(t+1|t)\|_Q^2 + \|\Delta \mathbf{U}_M(t)\|_W^2$$
 (5a)

s.t.
$$\hat{\mathbf{Y}}_P(t+1|t) = \Lambda_P \hat{\mathbf{Y}}(t|t) + A_P^M \Delta \mathbf{U}_M(t)$$
 (5b)

$$\Delta u_{min} \le \Delta \mathbf{U}_M(t) \le \Delta u_{max}$$
 (5c)

$$u_{min} \le \mathbf{U}_M(t) \le u_{max} \tag{5d}$$

where u_{max} , u_{min} , Δu_{max} , Δu_{min} are input constraints and increment constraints, respectively. The matrix A_P^M is the dynamic matrix with $P \times M$ block matrix and Λ_P is the shift matrix with appropriate dimension. Q,W are the weighting matrices for outputs and the controller moves. The above notations read

$$\begin{split} \hat{Y}_{P}(t+1|t) &= \left[\hat{y}^{T}(t+1|t),...,\hat{y}^{T}(t+P|t)\right]^{T}, \\ \Delta \mathbf{U}_{M}(t) &= \left[\Delta \mathbf{u}^{T}(t|t),...,\Delta \mathbf{u}^{T}(t+M-1|t)\right]^{T}, \\ R(t+1|t) &= \left[\mathbf{r}^{T}(t+1|t),...,\mathbf{r}^{T}(t+P|t)\right]^{T}, \\ \mathbf{r}^{T}(t+k|t) &= \left[r_{1}(t+k|t),...,r_{n_{y}}(t+k|t)\right]^{T}, \forall k \in \mathbb{I}_{1:P} \\ A_{P}^{M} &= \begin{bmatrix} A_{1} & 0 & \cdots & 0 \\ A_{2} & A_{1} & \cdots & 0 \\ \vdots & \ddots & \vdots \\ A_{M} & A_{M-1} & \cdots & A_{1} \\ \vdots & & & \\ A_{P} & A_{P-1} & \cdots & A_{P-M+1} \end{bmatrix}, \\ \Lambda_{P} &= \left[I_{P\cdot n_{y}\times P\cdot n_{y}} & \mathbf{0}\right] \times \Lambda, \\ Q &= diag(Q_{1},...,Q_{P}), Q_{1} = diag\{q_{1},...,q_{n_{y}}\} \\ \mathbf{W} &= diag(W_{1},...,W_{M}), W_{1} = diag\{w_{1},...,w_{n_{u}}\}. \end{split}$$

At every sample time, controller evaluates its future input trajectories by solving the optimization problem (5) and sends the first step of its entire future input trajectory to its actuators. However, although the future target information R(t+1|t) of the controlled variable were embedded in the optimization problem of DMC algorithm, the default choice in DMC algorithm was r(t+k|t) = r(t+1|t), $\forall k \in \mathbb{I}_{2:P}$. Little attention has been paid to the selection of an appropriate future trajectory horizon and the use of future target information.

3. Main Results

In this section, we first derive the explicit control law of the unconstrained MPC, which includes two parts: (i) the future target information feedforward, and (ii) the output feedback. Based on the future target information feedforward, we demonstrate that a poor future trajectory horizon has quite an impact on the system's performance. Then we propose an optimization method to determine the future trajectory horizon and the tripe-mode model predictive control using future target information. The triple-mode MPC is composed of the designed unconstrained control law and the extra degrees of freedom. The future target information is taken into account explicitly to improve tracking performance.

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3.1. Illustrations of Poor Future Trajectory Horizon

Now we show that the unconstrained MPC control law will provide possibilities in the explicit expression of feedforward and feedback. Consider the performance objective J(t) in problem (5), one can derive the unconstrained law by minimizing it w.r.t the future control moves, according the extremum condition $d(J(t))/d(\Delta \boldsymbol{U}_M(t)) = 0$, we have

$$\Delta \mathbf{U}_{M}(t) = ((A_{P}^{M})^{T} \mathbf{Q} A_{P}^{M} + \mathbf{W})^{-1} (A_{P}^{M})^{T} \mathbf{Q} (R(t+1|t) - \Lambda_{P} \hat{\mathbf{Y}}(t|t))$$
(6)

and making the following substitutions

$$F_r \leftarrow ((A_P^M)^T Q A_P^M + W)^{-1} (A_P^M)^T Q$$

$$K \leftarrow ((A_P^M)^T Q A_P^M + W)^{-1} (A_P^M)^T Q \Lambda_P$$
(7)

then we can get

$$\Delta u_M(t) = F_r R(t+1|t) - K \hat{\mathbf{Y}}(t|t)$$
(8)

It can be seen that the future target information is involved in the first term of the control law: $F_rR(t+1|t)$, which can be seen as the feedforward in the unconstrained control law. In addition, the second part of the control law can be seen as the output feedback based on the current output prediction.

For convenience, we define the future trajectory horizon in feedforward term for each output as $f_i \in \mathbb{R}, \forall i \in \mathbb{I}_{1:n_y}$, which indicates the length of future target information considered in the optimization. Any future targets beyond the future trajectory horizon will not be taken into account in the optimization problem, even if known. For a given $f_i, \forall i \in \mathbb{I}_{1:n_y}$, the future target information adopted in MPC can be expressed as

$$r_i(t+f_i+k|t) = r_i(t+f_i|t), \forall k \in \mathbb{I}_{1:P-f_i}$$
(9)

Furthermore, by combining the specific future trajectory horizon, the unconstrained law can be represented as follows:

$$F_r R(t+1|t) = F_1 r_1 + ... + F_{n_y} r_{n_y}$$

$$= \tilde{F}_1 \tilde{r}_1 + ... + \tilde{F}_{n_y} \tilde{r}_{n_y}$$
(10)

where $F_i r_i$, $\forall i \in \mathbb{I}_{1:n_y}$ refers to the ith feedforward contribution, and $\tilde{F}_i \tilde{r}_i$, $\forall i \in \mathbb{I}_{1:n_y}$ is the reconstructed future target information feedforward component based on the designed future trajectory horizon f_i .

$$F_{i} = \begin{bmatrix} F_{i}, F_{n_{y}+i}, ..., F_{(P-1) \cdot n_{y}+i} \end{bmatrix},$$

$$\tilde{F}_{i} = \begin{bmatrix} F_{i}, F_{n_{y}+i}, ..., F_{(f_{i}-2) \cdot n_{y}+i}, F_{(f_{i}-1) \cdot n_{y}+i} + ... + F_{(P-1) \cdot n_{y}+i} \end{bmatrix},$$

$$r_{i} = \begin{bmatrix} r_{i}(t+1|t) \\ r_{i}(t+2|t) \\ \vdots \\ r_{i}(t+P|t) \end{bmatrix}, \tilde{r}_{i} = \begin{bmatrix} r_{i}(t+1|t) \\ r_{i}(t+2|t) \\ \vdots \\ r_{i}(t+f_{i}|t) \end{bmatrix}, \forall i \in \mathbb{I}_{1:n_{y}}$$

and F_i , $\forall j \in \mathbb{I}_{1:P \cdot n_y}$ denotes the *j*th column vector of the feedforward matrix F_r .

It indicates that, for the ith output, the original P-dimension target vector \mathbf{r}_i has been replaced by a designed f_i -dimension vector $\tilde{\mathbf{r}}_i$. A major current focus in improving the control performance is how to select a proper f_i , $\forall i \in \mathbb{I}_{1:n_y}$. It is known that the typical DMC algorithm considers no setpoint changes during the optimizaiton, which is equivalent to set the future trajectory horizon as $f_i = 1$, $\forall i \in \mathbb{I}_{1:n_y}$.

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Next, we examine the closed-loop performances of the MPC algorithm adopting different choices of future trajectory horizon. Consider a single-input, single-output system described by the following transfer function

 $G(s) = \frac{1}{(10s+1)(5s+1)} \tag{11}$

The sampling time is chosen as 5 s, a step change of setpoint happens at sampling instant 15 and the unconstrained MPC algorithm is applied to drive the system to its target. The arbitrary choices of future trajectory horizon are f = 1, 6, 15. The tuning parameters of DMC are: P = 15, M = 3 and Q = I, R = 5 * I in which I is the identity matrix.

As illustrated by Figure 1, with a default choice of future trajectory horizon in MPC (f=1), the system response is slugglish when the setpoint changes, in contrast, setting the future trajectory horizon as the prediction horizon could result in an aggressive response. A proper selection f=6 deserves a desirable tracking performance.

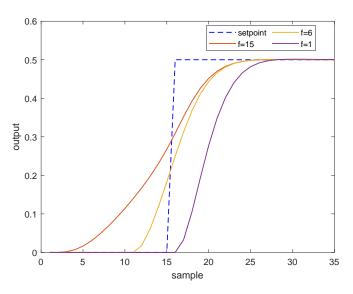


Figure 1. The closed-loop output response with respect to different future trajectory horizon.

The integral of squared error (ISE) criterion is widely used to evaluate the system performance in control engineering, the discrete form of ISE reads

$$ISE = \sum_{t=0}^{\infty} \left[error(t) \right]^2 \tag{12}$$

in which error(t) refers to the difference between the expected value (target value) and the actual response value at time instant t.

The ISE values shown in Table 1 demonstrate that the standard MPC algorithm with no anticipation (f = 1) owns large ISE value during the transition from one target to another. On the other hand, with large number of future trajectory horizon (f = 15), the system would react far in advance and lead to bad performance too.

Table 1. Closed-loop system performance with different choices of f.

	f = 1	f = 6	f = 15
ISE	0.8055	0.1797	0.3192

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3.2. Future Trajectory Horizon Optimization Algorithm

Since the closed-loop response with smaller ISE value is better, we advocate use of the ISE value to select the proper future trajectory horizon. The ISE value can be regarded as a function of future trajectory horizon, i.e., $ISE_i = g(f_i)$, $\forall i \in \mathbb{I}_{1:n_y}$. A better f_i deserves lower function value $g(f_i)$, we take the idea of golden section search algorithm [17] to optimize the future trajectory horizon. The algorithm can be summarized as follows:

According to Algorithm 1, we plot the ISE value subject to the iteration of a_k , b_k , λ_k , μ_k as Figure 2 shows. The optimal future trajectory horzion obtained is $f = \mu_6 = 6$. Which testifies the result of last section.

Algorithm 1 The optimization of Future trajectory horizon based on ISE value

For any controlled variable y_i , $\forall i \in \mathbb{I}_{1:n_y}$;

Step 1. Given the prediction horizon P, set $a_1 = 1$, $b_1 = P$, then calculate the initial point:

$$\lambda_1 = \lfloor a_1 + 0.382 * (b_1 - a_1) \rfloor$$

$$\mu_1 = \lceil a_1 + 0.618 * (b_1 - a_1) \rceil$$
(13)

and set k = 1;

Step 2. Give a specified target, govern the process by using the control law Equation (8) and evaluate the ISE value $g(\cdot)$ over the entire runtime;

Step 3. If $a_k == \lambda_k$, set $f_i = \mu_k$ or if $b_k == \mu_k$ set $f_i = \lambda_k$, and the optimal future trajectory horizon is obtained, break the optimization; Otherwise, if $g(\lambda_k) > g(\mu_k)$, go to Step 4, else if $g(\lambda_k) \leq g(\mu_k)$, go to Step 5;

Step 4. Set

$$\begin{cases}
a_{k+1} = \lambda_k \\
b_{k+1} = b_k \\
\lambda_{k+1} = \mu_k \\
\mu_{k+1} = \lceil a_{k+1} + 0.618 * (b_{k+1} - a_{k+1}) \rceil
\end{cases}$$
(14)

and go to Step 6;

Step 5. Set

$$\begin{cases}
 a_{k+1} = a_k \\
 b_{k+1} = \mu_k \\
 \mu_{k+1} = \lambda_k \\
 \lambda_{k+1} = \lfloor a_{k+1} + 0.382 * (b_{k+1} - a_{k+1}) \rfloor
\end{cases}$$
(15)

and go to Step 6;

Step 6. Set k = k + 1, go to Step 2.

3.3. Triple-Mode MPC Algorithm Using Future Target Information

For the conventional MPC algorithm, the optimization problem (5) is solved with $n_u \cdot M$ degree of freedom $\Delta \boldsymbol{U}_M(t)$ to tackle constraints. However, the original optimization problem treats the input as decision variables, which breaks down the inherent future target information feedforward structure as described before. What's more, the default choice of future trajectory horizon $f_i = 1, \forall i \in \mathbb{I}_{1:n_y}$ in the MPC algorithm may lead to sluggish tracking performance. There exists no effective method to determine a proper future target horizon for MPC optimization.

With the proposed Algorithm 1 used, we next present a triple-mode MPC algorithm using future target information. Different from the typical DMC algorithm as described in preliminary section, the proposed triple-mode control law encompasses three parts: (i) the future target information feedforward, (ii) the output feedback, and (iii) the extra degrees of freedom. Each mode of the control law can be designed individually. The first two parts of the control law are off-line designed through

unconstrained MPC, and the optimal future trajectory horizon is obtained by using Algorithm 1. The final part is calculated by the on-line MPC algorithm aiming to satisfy constraints.

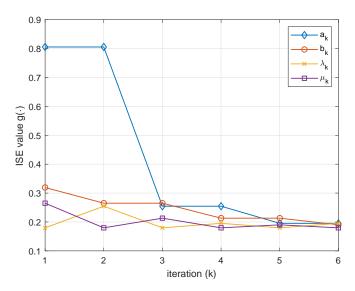


Figure 2. The evolution of golden section search for future trajectory horizon of illustrated example by using Algorithm 1.

Enhance the unconstrained MPC control law Equation (8) with an additional term $C(t) \in \mathbb{R}^{n_u \cdot M}$

$$\Delta \mathbf{U}_{M}(t) = F_{r}R(t+1|t) - K\hat{\mathbf{Y}}(t|t) + \mathbf{C}(t)$$
(16)

in which $C(t) = [c(t|t), c(t+1|t), ..., c(t+M-1|t)]^T$ and $c(t+i|t), i \in \mathbb{I}_{0:M-1} \in \mathbb{R}^{N_u}$ representing degrees of freedom to get the constraints satisfied.

It indicates that the original degree of freedom $\Delta U_M(t)$ in constrained DMC optimization (5) is replaced by C(t), which not only provide the feedforward design from future target information but also guarantee the advantage of constraint satisfaction. At each sampling time, the controller solves the following optimization problem

$$\min_{\boldsymbol{C}(t)} \|\boldsymbol{C}(t)\|_{W}^{2} \tag{17a}$$

s.t.
$$\hat{\mathbf{Y}}_{P}(t+1|t) = \Lambda_{P}\hat{\mathbf{Y}}(t|t) + A_{P}^{M}\Delta\mathbf{U}_{M}(t)$$
 (17b)

$$\Delta \mathbf{U}_{M}(t) = F_{r}R(t+1|t) - K\hat{\mathbf{Y}}(t|t) + C(t)$$
(17c)

$$\Delta u_{min} \le \Delta \mathbf{U}_M(t) \le \Delta u_{max} \tag{17d}$$

$$u_{min} \le \mathbf{U}_M(t) \le u_{max} \tag{17e}$$

$$\hat{\mathbf{Y}}_{P}(t+P|t) = R(t+P|t) \tag{17f}$$

where Equation (17f) refers to the terminal constraint used to ensure closed-loop stability when model predictive control is employed. After optimization, the optimal solution $C^*(t) = [c^*(t|t), c^*(t+1|t), ..., c^*(t+M-1|t)]^T$ can be obtained, and the optimal input increment is nothing but $\Delta u^*(t) = d^T(F_rR(t+1|t) - K\hat{Y}(t|t)) + c^*(t|t)$ with $d = [I_{n_u}, \mathbf{0}, ..., \mathbf{0}]^T$. Note that the proposed triple-mode MPC optimization problem (17) is a quadratic programming [18] with $n_u \times M$ degrees of freedom. The degrees of freedom are the same as the original DMC optimization problem (5), thus the computation load of proposed triple-mode MPC is the same as which of DMC.

A detailed implementation procedure of the proposed triple-mode MPC algorithm (Algorithm 2) is summarized as follows.

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Algorithm 2 Triple-mode MPC algorithm using future target information

Offline computation:

Carry out the Algorithm 1 to obtain the future trajectory horizon f_i , $\forall i \in \mathbb{R}^{n_y}$, the first two parts of the control law are designed through Equations (7) and (10);

Online computation:

Step 1. At sampling time t, controller receives measurement from the sensors and evaluate the modified estimate of predictions according to Equation (4);

Step 2. Solve the optimization problem (17) to evaluate its future input trajectory;

Step 3. Injects the optimal input into the plant;

Step 4. Set t = t + 1, and go to Step 1.

In this section, the triple-mode MPC using future target information is presented. As has been previously stated, this triple-mode control law is based on the usage of the perturbations on the fixed dual-mode unconstrained control law. To this end, the following assumption is considered.

Assumption 1. The step response sequence $a_{i,j,k}$, $\forall i \in \mathbb{I}_{1:n_y}$, $\forall j \in \mathbb{I}_{1:n_u}$, $\forall k \in N_+$ is a Cauchy sequence: $\forall \epsilon > 0, \exists N \in \mathbb{N}, \forall n, \forall m, (m, n > N \to |a_{i,j,n} - a_{i,j,m}| < \epsilon)$.

Assumption 2. The weighting matrices $Q \in \mathbb{R}^{P \cdot n_y \times P \cdot n_y}$ and $R \in \mathbb{R}^{M \cdot n_u \times M \cdot n_u}$ are positive definite matrices. At least as many inputs as outputs is required: $n_u \ge n_y$.

The future target is admissible if there exist a set of control sequence $\Delta \boldsymbol{U}_M(t)$ such that the system output $\hat{\boldsymbol{Y}}_P(t)$ can reach it and the constraints (e.g., $\Delta u_{min} \leq \Delta \boldsymbol{U}_M(t) \leq \Delta u_{max}$, $u_{min} \leq \boldsymbol{U}_M(t) \leq u_{max}$) can be satisfied during the stage. The following theorem follows immediately.

Theorem 1. Consider that Assumption 1 and 2 hold, and the future target R(t+1|t) is admissible. Then, for any feasible initial state $\hat{\mathbf{Y}}(t|t)$, the proposed triple-mode controller $\Delta u^*(t) = d^T(F_rR(t+1|t) - K\hat{\mathbf{Y}}(t|t)) + c^*(t|t)$ asymptotically steers the system to R(t+1|t).

The proof can be found in the Appendix A.

4. Applications

In this section, dynamic simulations are carried out to evaluate the performance of the proposed triple-mode controllers. This section presents two illustrative applications for the proposed methodology: (i) the shell fundamental control problem (case study I), and (ii) the coordinated control problem in the power plants (case study II). We aim at showing the better performance can be achieved by proper selection of future trajectory horizon. The simulation case study was performed on a PC with Intel Core i5 Quad 1.6GHz, 16GB memory and in the Matlab platform.

4.1. System I: A Heavy Oil Fractionator

In this example, consider a plant shown in Figure 3 presented in Prett and Morari [19]. in which a gaseous feed stream is separated by removing heat.

Here we will only consider the two-by-two subsystem, which consists of two inputs: the top draw u_1 and the side draw u_2 ; two outputs: the top end point y_1 and the side end point y_2 . The model for this system is:

$$\begin{bmatrix} y_1 \\ y_2 \end{bmatrix} = \begin{bmatrix} \frac{4.05e^{-30s}}{50s+1} & \frac{1.77e^{-30s}}{60s+1} \\ \frac{5.39e^{-20s}}{50s+1} & \frac{5.72e^{-15s}}{60s+1} \end{bmatrix} \begin{bmatrix} u_1 \\ u_2 \end{bmatrix}$$
 (18)

The system will be represented using a 60-coefficient step response model with a 5-min sampling time. Set the initial operating point to be the origin and the upper bound of both output and input is 0.5, the lower bound of both output and input is -0.5. Three MPC algorithms are used to compare the

system performance: the typical DMC, the proposed triple-mode MPC (Algorithm 2), and the DMC algorithm with an artificial selection of future target horizon (denoted as DMC-FF in the following). Tuning parameters of the MPC controllers are the same as follows: a prediction horizon of P=60 and a control horizon of M=8. The weighting matrices are set as identity matrix. In the DMC-FF algorithm, the future target horizon is selected as $f_1=40$, $f_2=40$. In the triple-mode MPC algorithm, the optimal future target horizon can be obtained as $f_1=13$, $f_2=13$ according to Algorithm 1. To compare the tracking performance, the evolution of setpoint is given as: the initial setpoint is coincident with the system's initial operating point; at sample time 20, change the setpoint sp_1 of output y_1 to its upper bound and the setpoint sp_2 of output y_2 is also changed to its upper bound when sample time 40; at sample time 60, set the setpoint of output y_1 to the origin and the setpoint of output y_2 is also set to the origin at sample time 80.

Figures 4 and 5 present the output response and input response of the controlled system.

As it can be seen in Figure 4, both two outputs are sluggish under the typical DMC algorithm when the setpoint changed. On the other hand, using an artificial selection of future target horizon may cause the system to response to the future target information far in advance. The performance is degraded because the typical DMC algorithm overlooks the information of future target and the DMC-FF algorithm uses too much future target information. In contrast, the triple-mode MPC algorithm which taking into account the future target information properly can respond to subtlety, the performance of the system is improved dramatically.

Next, Table 2 shows the sum of the ISE value of the controlled system for each control strategy throughout the simulation horizon. The DMC-FF using the future target information can outperform the typical DMC, and the triple-mode MPC using an optimal future target horizon achieves the best tracking performance among the three algorithms.

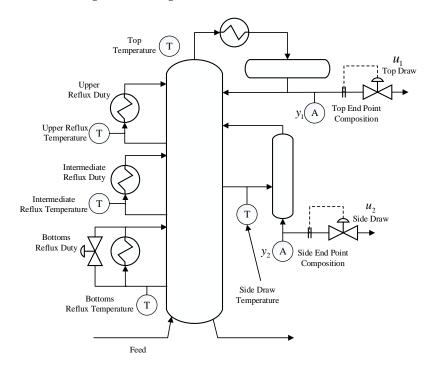


Figure 3. Schematic diagram of "Shell" heavy oil fractionator [5]. Reproduced with permission from J.M.Maciejowski, predictive control with constraints; published by Pearson education, 2002.

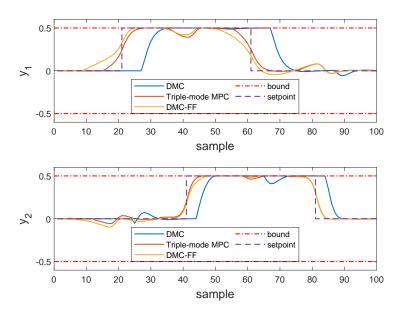


Figure 4. Comparison of output response obtained by DMC, triple-mode MPC and DMC-FF. The top end point is contained in the first panel and the side end point is contained in the second panel.

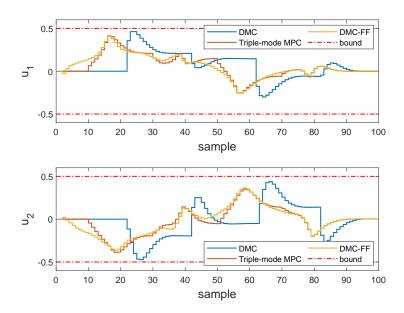


Figure 5. Comparison of input response obtained by DMC, triple-mode MPC and DMC-FF. The top draw is contained in the first panel and the side draw is contained in the second panel.

Table 2. Comparison of tracking error with respect to typical DMC, the triple-mode MPC and the DMC-FF algorithms.

	DMC	Triple-Mode MPC	DMC-FF
ISE	6.3771	0.7088	0.9515

4.2. System II: A Power Plant Coordinated Control System

Coordinated control system (CCS) is the system that coordinates the steam turbine and the boiler at the same time to respond to the various load demands quickly [20]. The boiler and the turbine possess different dynamic characteristics. The dynamic from the combustion rate to the main steam pressure is a slow process with large delay and great inertia. In contrast, the response from the turbine governor valve to the unit output is a relatively fast process.

The simplified coordinated control system can be shown in Figure 6.

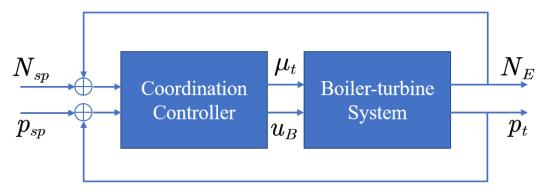


Figure 6. Simplified block diagram of the coordinated control system.

It can be seen that this system is a two-input, two-output control system, in which the manipulated variables are the fuel command $u_B(\%)$ and the opening level of the turbine valve $\mu_t(\%)$, the controlled variables are the main steam pressure $p_t(MPa)$ and the output power $N_E(MW)$. Consider a 660MW unit in Datang Panshan Power Plant, China, in which the CCS is composed of the boiler of Type HG - 2023/17.6 - YM4 boiler and the turbine of Type N600 - 16.7/537/537 - I. The nonlinear model from the load 50% to load 100% was identified through the step test [21]. When the load $N_E = 550MW$, the linearized model is:

$$\begin{bmatrix} \Delta N_E \\ \Delta p_t \end{bmatrix} = \begin{bmatrix} \frac{2257s}{(1+250s)(1+12s)} & \frac{18.6(1-35s)}{(1+189s)(1+250s)(1+12s)} e^{-23s} \\ \frac{-0.279}{1+250s} & \frac{0.571(1-35s)}{(1+189s)(1+250s)} e^{-23s} \end{bmatrix} \begin{bmatrix} \Delta \mu_t \\ \Delta u_B \end{bmatrix}$$
(19)

In this case study, it was established that the control system must always obey the speed restriction on the manipulated variables $|\Delta\mu_t|\leq 0.5\%$, $|\Delta u_B|\leq 0.5\%$, and the system is initially at $N_E=550$ MW, $p_t=16.9$ Mpa. The sampling time is T=5 s. Three MPC algorithms are used to compare the system performance: the typical DMC, the proposed triple-mode MPC (Algorithm 2), and the DMC algorithm with an artificial selection of future target horizon (denoted as DMC-FF in the following). Tuning parameters of the three MPC algorithms are the same as follows: the prediction horizon is P=300 and the control horizon is P=3000 and the control horizon is P=3000; the weighting matrices are set as: the weight for P_E is P_E and for P_E is P_E and P_E are set to P_E and P_E are set to design the feedforward based on Algorithm 1. The main purpose of the CCS is to keep the output power responding to load demands quickly when the unit running in either constant or sliding pressure operation. The following two scenarios are considered:

4.2.1. Constant Pressure Operation

When the unit is running in constant pressure operation mode, the main steam pressure is maintained at the rated value regardless of any changes in load demand.

Assuming that the evolution of load demand is given as: the initial load demand is coincident with the system's initial operating point $N_E = 550$ MW; at sample time 200, change the load demand to 600 MW then remain constant; at sample time 700, set the target load to 500 MW and then push it

to the 550 MW at time instant 1500. In order to prevent the step load disturbance of the target load from impacting the entire control system of the unit, the setpoint of the output power is formed by limiting the load change rate after the target load is changed [22]. In general, the load change rate is determined by the operating personnel according to the operating conditions of the unit equipment. Here we set the load change rate as 5 MW/min.

Figure 7 presents the dynamics of the controlled outputs N_E and p_t . The figure shows the responses obtained by the typical DMC, the triple-mode MPC and the DMC-FF algorithms. The control actions implemented by the manipulated inputs μ_t and u_B that caused the responses in Figure 7, are shown in Figure 8.

It can be observed the output power governed by triple-mode MPC can track the load demand more quickly while maintaining steam pressure at the constant value. In contrast, the DMC-FF algorithm uses too much future target information and responses to the load demand far in advance, which leads to large oscillations in the main steam pressure. The main steam pressure controlled by the typical DMC algorithm also oscillates a lot when the load demand changes. In this case, the typical DMC algorithm even outperforms the DMC-FF algorithm due to the improper selection of future target horizon in the DMC-FF algorithm.

Table 3 reports the square errors between the output response and the desired setpoint value. In contrast, the proposed triple-mode MPC is expressed explicitly in terms of future information feedforward, and is hence expected to yield improved results for tracking performance.

	Error of N_E (MW)	Error of p_t (MPa)
DMC	431.7057	5.6357
Triple-mode MPC	104.3930	0.0331
DMC-FF	877.6251	32.3255

Table 3. Comparison of square errors under constant pressure operation.

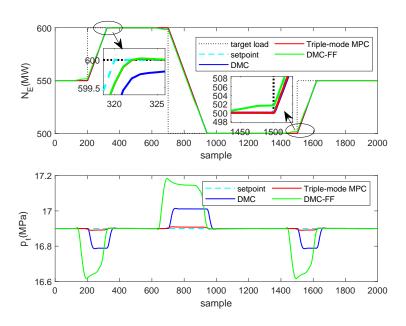


Figure 7. Comparison of output response. The output power N_E is contained in the first panel and the main steam pressure p_t is contained in the second panel.

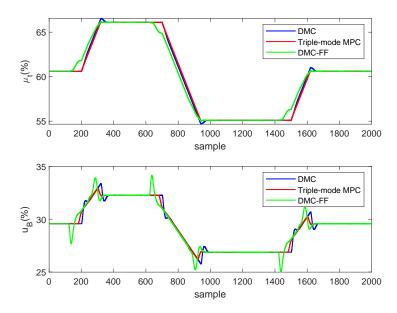


Figure 8. Comparison of input response. The turbine valve μ_t is contained in the first panel and the fuel command u_B is contained in the second panel.

4.2.2. Sliding Pressure Operation

We then proceed with the running of the unit concerning sliding pressure operation, and the optimal operating curve is plotted in Figure 9. The main steam pressure increases in line with the increase of the load when the load is less than 550 MW, and maintains constant when the load exceeds 550 MW. The load demands used for tracking are the same as before.

Figure 10 presents the dynamics of the controlled outputs N_E and p_t . The figure shows the responses obtained by the typical DMC, the proposed triple-mode MPC and the DMC-FF algorithms. The control actions implemented by the manipulated inputs μ_t and u_B that caused the responses in Figure 10, are shown in Figure 11.

Analyzing the results in the first panel of Figure 10, one can notice that for the trajectory of the controlled output N_E under the proposed triple-mode MPC algorithm is closer to the desired trajectory than which under the typical DMC algorithm. In addition, the trajectory governed by the DMC-FF algorithm can also respond to the load demand more quickly than the typical DMC algorithm. (The curves of triple-mode MPC and DMC-FF almost overlap in the left magnified figure) However, the DMC-FF algorithm responses to the load demand far too early, which leads to the loss of tracking performace as we can see in the right magnified figure.

On the other hand, as shown in the second panel of Figure 10, when the setpoint of the main steam pressure changes with the load demand, the accuracy of tracking deteriorates a lot under either the typical DMC or the DMC-FF algorithms. In contrast, using the triple-mode MPC can drive the main steam pressure p_t to track its setpoint without too much performance loss.

A quantitative comparison of square errors for the whole simulation is also shown in Table 4. In the table, the power output and pressure errors of the triple-mode MPC algorithm are dramatically reduced compared to those of the typical DMC and the DMC-FF algorithms.

Table 4. Comparison of square errors under sliding pressure operation.

	Error of N_E (MW)	Error of p_t (MPa)
DMC	501.7570	10.7935
Triple-mode MPC	124.5650	0.1009
DMC-FF	753.2611	22.1475

Remark 1. In many practical processes such as power plants [23], wind tunnels [24], there exists future target information that can be used in feedforward design. When the MPC algorithm is applied to real systems, the closed-loop performance is related to the accuracy of the model and the future target information. If the model is consistent with the plant, and the future target information is correct, the control performance obtained is as good as which obtained in the case study.

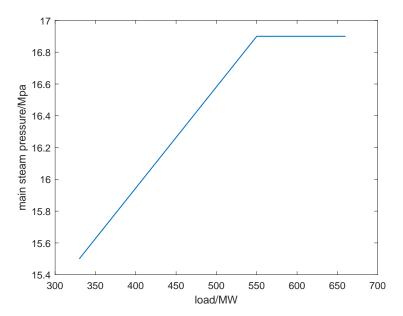


Figure 9. Sliding pressure operation curve of the 660 MW unit.

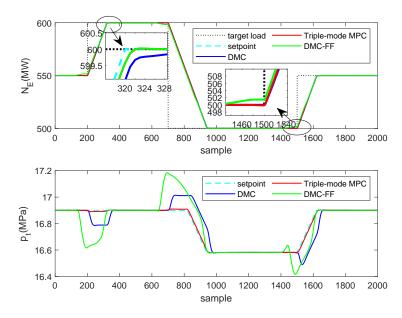


Figure 10. Comparison of output response. The output power N_E is contained in the first panel and the main steam pressure p_t is contained in the second panel.

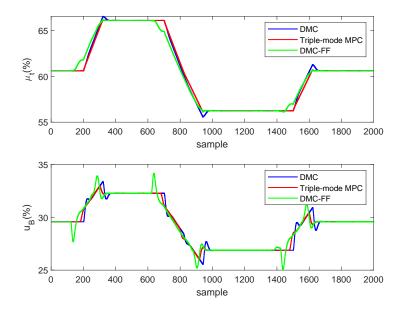


Figure 11. Comparison of input response. The turbine valve μ_t is contained in the first panel and the fuel command u_B is contained in the second panel.

5. Conclusions

In this work, we propose a triple-mode model predictive control algorithm using future target information. In order to explicitly take into account the future target information in the MPC optimization, the proposed triple-mode control law includes the future target information feedforward term, and the future trajectory horizon can be optimized off-line to design the feedforward. Furthermore, the extra degrees of freedom are added to append the control law such that the constraints can be met when the MPC is running. Experimental results on the shell fundamental control problem, and the coordinated control problem in the power plant demonstrate that, by incorporating future target information feedforward explicitly and using an optimal future target horizon, the proposed triple-mode MPC algorithm could better hedge against the future target information, mitigate the sluggish response, and improve the tracking performance.

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Appendix A. Proof of Theorem 1

Proof of Theorem 1. A deviation model is obtained by computing an error model with respect to the future targets. To do so, consider a desired future trajectory described by R(t+1|t), and define deviation variables

$$\bar{\mathbf{Y}}_{P}(t+1|t) = \hat{\mathbf{Y}}_{P}(t+1|t) - R(t+1|t)$$
(A1)

that satisfy the dynamic model

$$\bar{\mathbf{Y}}_{P}(t+1|t) = \Lambda_{P}\bar{\mathbf{Y}}(t|t) + A_{P}^{M}\Delta\mathbf{U}_{M}(t) \tag{A2}$$

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The zero regulation problem applied to the system in deviation variables finds $\Delta U_M(t)$ that takes $\bar{Y}(t|t)$ to zero.

Feasibility: Assume that the state at the current sample time t is $\bar{Y}(t|t)$. Also assume that the optimal solution is $C^*(t) = [c^*(t|t), c^*(t+1|t), ..., c^*(t+M-1|t)]^T$ with an optimal cost $V^*(\bar{Y}(t|t), C^*(t))$. Let $\bar{Y}(t+1|t)$ be the state at the next sampling time. Consider a control sequence

$$\Delta \tilde{\mathbf{U}}_{M}(t+1) = F_{r}R(t+2|t+1) - K\hat{\mathbf{Y}}(t+1|t+1) + \tilde{\mathbf{C}}(t+1)$$
(A3)

with $\tilde{C}(t+1) = [c^*(t+1|t), ..., c^*(t+M-1|t), \mathbf{0}]^T$. Then it is easy to see that $\Delta \tilde{\mathbf{U}}_M(t+1)$ is a feasible solution at time t+1 due to the feasibility of the optimal solution at time t and enforced terminal constraint. Consequently, $\hat{\mathbf{Y}}_P(t+1+P|t+1) = R(t+1+P|t+1)$.

Convergence: Consider the feasible solution at time t + 1 previously presented. Following standard steps in the stability proofs of MPC (Mayne et al. [25]), we get that

$$V^{*}(\bar{\mathbf{Y}}(t+1|t+1), C^{*}(t+1))$$

$$\leq V(\bar{\mathbf{Y}}(t+1|t+1), \tilde{C}(t+1))$$

$$\leq V^{*}(\bar{\mathbf{Y}}(t|t), C^{*}(t)) - \|\mathbf{r}(t+1|t) - \hat{\mathbf{y}}^{*}(t+1|t)\|_{q}^{2} - \|\Delta \mathbf{u}^{*}(t|t)\|_{w}^{2}$$
(A4)

Due to the definite positiveness of the optimal cost and its nonincreasing evolution, we infer that $\lim_{t\to\infty} \|\bar{Y}_P(t+1|t)\|_Q^2 = 0$ and $\lim_{t\to\infty} \|\Delta \boldsymbol{U}_M(t)\|_W^2 = 0$. Consequently, the system is steered to R(t+1|t). \square

References

- 1. Qin, S.J.; Badgwell, T.A. A survey of industrial model predictive control technology. *Control Eng. Pract.* **2003**, 11, 733–764. [CrossRef]
- 2. Garcia, C.E.; Morshedi, A. Quadratic programming solution of dynamic matrix control (QDMC). *Chem. Eng. Commun.* **1986**, *46*, 73–87. [CrossRef]
- 3. Rawlings, J.B. Tutorial overview of model predictive control. IEEE Control Syst. Mag. 2000, 20, 38–52.
- 4. Rawlings, J.B.; Mayne, D.Q. *Model Predictive Control: Theory and Design*; Nob Hill Pub.: San Francisco, CA, USA, 2009.
- 5. Maciejowski, J.M. Predictive Control: With Constraints; Pearson Education: London, UK, 2002.
- 6. Goodwin, G.; Seron, M.M.; De Doná, J.A. *Constrained Control and Estimation: An Optimisation Approach*; Springer Science & Business Media: Berlin, Germany, 2006.
- 7. Zhang, K.; Zhao, J.; Zhu, Y. MPC case study on a selective catalytic reduction in a power plant. J. Process Control 2018, 62, 1–10. [CrossRef]
- 8. Di Carlo, J.; Wensing, P.M.; Katz, B.; Bledt, G.; Kim, S. Dynamic locomotion in the mit cheetah 3 through convex model-predictive control. In Proceedings of the 2018 IEEE/RSJ International Conference on Intelligent Robots and Systems (IROS), Madrid, Spain, 1–5 October 2018; pp. 1–9.
- 9. Limón, D.; Alvarado, I.; Alamo, T.; Camacho, E.F. MPC for tracking piecewise constant references for constrained linear systems. *Automatica* **2008**, *44*, 2382–2387. [CrossRef]
- 10. Clarke, D.W.; Mohtadi, C. Properties of generalized predictive control. *Automatica* **1989**, 25, 859–875. [CrossRef]
- 11. Middleton, R.H.; Chen, J.; Freudenberg, J.S. Tracking sensitivity and achievable performance in preview control. *Automatica* **2004**, *40*, 1297–1306. [CrossRef]
- Carrasco, D.S.; Goodwin, G.C. Feedforward model predictive control. *Annu. Rev. Control* 2011, 35, 199–206.
 [CrossRef]
- 13. Rossiter, J.; Grinnell, B. Improving the tracking of generalized predictive control controllers. *Proc. Inst. Mech. Eng. Part I J. Syst. Control Eng.* **1996**, 210, 169–182. [CrossRef]
- 14. Dughman, S.; Rossiter, J. Systematic and effective embedding of feedforward of target information into MPC. *Int. J. Control* **2017**, 1–15. [CrossRef]

Processes 2020, 8, 54 18 of 18

15. Valencia-Palomo, G.; Rossiter, J.; López-Estrada, F. Improving the feed-forward compensator in predictive control for setpoint tracking. *ISA Trans.* **2014**, *53*, 755–766. [CrossRef] [PubMed]

- 16. Qin, S.J.; Badgwell, T.A. *An Overview of Industrial Model Predictive Control Technology*; AIChE Symposium Series; American Institute of Chemical Engineers: New York, NY, USA, 1997; Volume 93, pp. 232–256.
- 17. Kiefer, J. Sequential minimax search for a maximum. Proc. Am. Math. Soc. 1953, 4, 502–506. [CrossRef]
- 18. Boyd, S.; Vandenberghe, L. Convex Optimization; Cambridge University Press: Cambridge, UK, 2004.
- 19. Prett, D.M.; Morari, M. The Shell Process Control Workshop; Elsevier: Amsterdam, The Netherlands, 2013.
- 20. Moon, U.C.; Lee, Y.; Lee, K.Y. Practical dynamic matrix control for thermal power plant coordinated control. *Control Eng. Pract.* **2018**, *71*, 154–163. [CrossRef]
- 21. Jizhen, L.; Liang, T.; Deliang, Z.; Xinping, L. Analysis on the Nonlinearity of Load-Pressure Characteristics of a 660MW Unit. *Power Eng.* **2005**, 25, 533–536.
- 22. Wood, A.J.; Wollenberg, B.F.; Sheblé, G.B. *Power Generation, Operation, and Control*; John Wiley & Sons: Hoboken, NJ, USA, 2013.
- 23. Flynn, D. Thermal Power Plant Simulation and Control; Number 43; IET: London, UK, 2003.
- 24. Green, J.; Quest, J. A short history of the European Transonic Wind Tunnel ETW. *Prog. Aerosp. Sci.* **2011**, 47, 319–368. [CrossRef]
- 25. Mayne, D.Q.; Rawlings, J.B.; Rao, C.V.; Scokaert, P.O. Constrained model predictive control: Stability and optimality. *Automatica* **2000**, *36*, 789–814. [CrossRef]



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