# A Numerical Approach to Solve Volume-Based Batch Crystallization Model with Fines Dissolution Unit 

## Authors:

Safyan Mukhtar, Muhammad Sohaib, Ishfaq Ahmad

Date Submitted: 2019-09-23

Keywords: orthogonal polynomials, quadrature method of moments, volume-based population balance model with fines dissolution

Abstract:

In this article, a numerical study of a one-dimensional, volume-based batch crystallization model (PBM) is presented that is used in numerous industries and chemical engineering sciences. A numerical approximation of the underlying model is discussed by using an alternative Quadrature Method of Moments (QMOM). Fines dissolution term is also incorporated in the governing equation for improvement of product quality and removal of undesirable particles. The moment-generating function is introduced in order to apply the QMOM. To find the quadrature abscissas, an orthogonal polynomial of degree three is derived. To verify the efficiency and accuracy of the proposed technique, two test problems are discussed. The numerical results obtained by the proposed scheme are plotted versus the analytical solutions. Thus, these findings line up well with the analytical findings.

Record Type: Published Article
Submitted To: LAPSE (Living Archive for Process Systems Engineering)
Citation (overall record, always the latest version): LAPSE:2019.1032
Citation (this specific file, latest version): LAPSE:2019.1032-1
Citation (this specific file, this version):
LAPSE:2019.1032-1v1
DOI of Published Version: https://doi.org/10.3390/pr7070453
License: Creative Commons Attribution 4.0 International (CC BY 4.0)

## Article

# A Numerical Approach to Solve Volume-Based Batch Crystallization Model with Fines Dissolution Unit 

Safyan Mukhtar ${ }^{1, *}$, Muhammad Sohaib ${ }^{2}$ and Ishfaq Ahmad ${ }^{2}$<br>1 Department of Basic Sciences, Deanship of Preparatory Year, King Faisal University, 31982 Hofuf, Al Ahsa, Saudi Arabia<br>2 Department of Mathematics \& Statistics, Bacha Khan University, 24461 Palosa, Charsadda Khyber Pakhtunkhwa, Pakistan<br>* Correspondence: smahmad@kfu.edu.sa; Tel.: +966-552825413

Received: 11 June 2019; Accepted: 12 July 2019; Published: 15 July 2019


#### Abstract

In this article, a numerical study of a one-dimensional, volume-based batch crystallization model (PBM) is presented that is used in numerous industries and chemical engineering sciences. A numerical approximation of the underlying model is discussed by using an alternative Quadrature Method of Moments (QMOM). Fines dissolution term is also incorporated in the governing equation for improvement of product quality and removal of undesirable particles. The moment-generating function is introduced in order to apply the QMOM. To find the quadrature abscissas, an orthogonal polynomial of degree three is derived. To verify the efficiency and accuracy of the proposed technique, two test problems are discussed. The numerical results obtained by the proposed scheme are plotted versus the analytical solutions. Thus, these findings line up well with the analytical findings.


Keywords: volume-based population balance model with fines dissolution; quadrature method of moments; orthogonal polynomials

## 1. Introduction

Population balance models (PBMs) show a significant role in different areas of science and engineering. These models have numerous applications in high-energy physics, geophysics, biophysics, meteorology, pharmacy, food science, chromatography, chemical engineering, civil engineering, and environmental engineering. These models are used in the process of cell dynamics, polymerization, cloud formation, and crystallization. In biophysics, these models are concerned with population of various kinds of cells. Population balance models are also used in the formation of ceramics mixtures and nanoparticles which have a lot of applications.

In 1964, Hulburt \& Katz [1] were first to discuss the PBMs in chemical engineering. A detailed description of these models is given in [2]. The main components in the models are the process of nucleation, growth, aggregation, breakage, inlet, outlet, growth, and dissolution. The mathematical model of population balance equations are partial integro-differential equations (PIDEs). Analytical solutions of these PIDEs are very rare except for a few simple cases. Therefore, researchers are interested in developing numerical solutions for these equations. Numerous numerical methods are accessible in the literature to solve certain kinds of PBMs; see, for example, [3-11].

The Quadrature Method of Moments (QMOM) for solving the governed models was first introduced by McGraw [12]. The direct QMOM was proposed by Fan et al. [4]. In addition, a new QMOM has been proposed by Gimbun [5]. Qamar et al. [13] introduced an alternative QMOM for solving length-based batch crystallization models telling crystals nucleation, size-dependent growth, aggregation, breakage, and dissolution of small nuclei below certain critical size. Safyan et al. [14] followed the technique of [13] for solving volume-based batch crystallization model nucleation,
size-dependent growth, aggregation, breakage. In this article, the QMOM is used to solve volume-based batch crystallization models with fines dissolution. The fines dissolution unit improves the product quality and removes unwanted particles.

In the proposed method, orthogonal polynomials, taken from the lower-order moments, are used to find the quadrature points and weights. For confirming accuracy of the scheme, a third-order orthogonal polynomial, employing the first six moments, was chosen to estimate the quadrature points (abscissas) and equivalent quadrature weights. Hence, it was essential to solve at least a six-moment system (i.e., $0, \ldots, 5$ ). This type of polynomial provides a three-point Gaussian quadrature rule which usually produces precise output for polynomials of degree five or less. The expression for the preferred orthogonal polynomial can be derived analytically and the mandatory number of moments rises with order of polynomial. It is important to mention that the calculation of six moments to generate each time the third-order polynomial is compulsory. However, the technique itself is not limited to the calculation of every listed number of moments. The calculation of additional moments is conducted by adding ordinary differential equation.

This article is divided into two parts: In the first part, the mathematical model of volume-based Population Balance Equation (PBE) with fines dissolution is presented. In the second part, the proposed QMOM is derived for PBEs. Furthermore, the mathematical outcomes of QMOM are compared with the analytical outcomes that are accessible in literature.

## 2. Materials and Methods

Suppose $u_{d}$ represents the number density function, then a general PBE is given by [1,2]:

$$
\frac{\partial u_{d}\left(T, V_{p}\right)}{\partial T}=-\underbrace{\frac{\partial\left[G\left(T, V_{p}\right) u_{d}\left(T, V_{p}\right)\right]}{\partial V_{p}}}_{\text {Growth-term }}+\underbrace{Q_{d}\left(0, V_{p}\right)=u_{d 0}\left(V_{p}\right)}_{\text {Nucleation-term }} \begin{gather*}
\text { Aggregation-term }\left(T, V_{p}\right)  \tag{1}\\
Q_{\text {agg }}^{ \pm}\left(T, V_{p}\right) \in R_{+}^{2}
\end{gather*} \underbrace{Q_{\text {break }}^{ \pm}\left(T, V_{p}\right)}_{\text {Breakage-term }}+\underbrace{Q_{\text {diss }}\left(T, V_{p}\right)}_{\text {Dissolution-term }}
$$

where $\mathbb{R}_{+}=(0, \infty)$. The variable $T$ represents the time and $V_{p}$ may be size, length, or composition. In this article, it represents the particle volume. In the above equation, each term has its specific definition. These terms are given by

$$
\begin{equation*}
Q_{\mathrm{agg}}^{ \pm}\left(T, V_{p}\right)=B_{\mathrm{agg}}\left(T, V_{p}\right)-D_{\mathrm{agg}}\left(T, V_{p}\right) \tag{2}
\end{equation*}
$$

where

$$
B_{\mathrm{agg}}\left(T, V_{p}\right)=\frac{1}{2} \int_{0}^{V_{p}} \beta\left(T, V_{p}-V_{p}^{\prime}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}-V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime}
$$

and

$$
D_{\mathrm{agg}}\left(T, V_{p}\right)=\int_{0}^{\infty} \beta\left(T, V_{p}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime}
$$

Here, $B_{\text {agg }}\left(T, V_{p}\right)$ represents the birth of particles of volume $V_{p}$ resulting for amalgamation of two particles with respective volume $V_{p}^{\prime}$ and $V_{p}-V_{p}^{\prime}$, where $V_{p}^{\prime} \in\left(0, V_{p}\right)$ and $D_{\mathrm{agg}}\left(T, V_{p}\right)$ is the death of particles, describing the decrease in particle volume $V_{p}$ by aggregation with other particles of any volume. The aggregation kernel $\beta\left(T, V_{p}, V_{p}^{\prime}\right)$ is the rate at which aggregation of two particles $V_{p}$ and $V_{p}^{\prime}$ produces a particle volume $V_{p}+V_{p}^{\prime}$.

$$
\begin{equation*}
Q_{\text {break }}^{ \pm}\left(T, V_{p}\right)=B_{\text {break }}\left(T, V_{p}\right)-D_{\text {break }}\left(T, V_{p}\right) \tag{3}
\end{equation*}
$$

where

$$
B_{\text {break }}\left(T, V_{p}\right)=\int_{V_{p}}^{\infty} b\left(T, V_{p}, V_{p}^{\prime}\right) S\left(V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime}
$$

and

$$
D_{\text {break }}\left(T, V_{p}\right)=S\left(V_{p}\right) u_{d}\left(T, V_{p}\right)
$$

Here, $B_{\text {break }}\left(T, V_{p}\right)$ represents the birth of new particles during the breakage process and the breakage function $b\left(T, V_{p}, V_{p}^{\prime}\right)$ is the probability density function for the formation of particle volume $V_{p}$ from particle volume $V_{p}^{\prime}$, whereas, $D_{\text {break }}\left(T, V_{p}\right)$ is the death of particles, and $S\left(V_{p}^{\prime}\right)$ is the selection function describing the rate at which the particles are selected to break.

$$
\begin{equation*}
Q_{\mathrm{diss}}\left(T, V_{p}\right)=\frac{\dot{V}}{V_{c}} h\left(V_{p}\right) u_{d}\left(T, V_{p}\right) \tag{4}
\end{equation*}
$$

$Q_{\text {diss }}\left(T, V_{p}\right)$ represents the dissolution term, $V_{c}$ is the volume of crystallizer, $\dot{V}$ is the volumetric flow rate from the crystallizer to dissolution unit, $h\left(V_{p}\right)$ is the dissolution function describing dissolution of small particles below some critical size. The population balance equation can be simplified through introducing the moment function. The $k^{t h}$ moment of the population density function is mathematically written in the form:

$$
\begin{equation*}
m_{k}(T)=\int_{0}^{\infty} V_{p}^{k} u_{d}\left(T, V_{p}\right) d V_{p} \tag{5}
\end{equation*}
$$

The first and second moments $m_{0}(T), m_{1}(T)$ denote particle population and volume, respectively, at any instant $T$. Multiply $V_{p}^{k}$ to left- and right-hand side of Equation (1) and at that moment integrate it over the volume $V_{p}$, so we obtain the following equation:

$$
\begin{equation*}
\frac{d m_{k}(T)}{d T}=\overline{G_{\text {growth }}}\left(T, V_{p}\right)+\overline{Q_{\text {nucleation }}}\left(T, V_{p}\right)+\overline{Q_{\text {aggregation }}}\left(T, V_{p}\right)+\overline{Q_{\text {breakage }}}\left(T, V_{p}\right)+\overline{Q_{\text {dissolution }}}\left(T, V_{p}\right) \tag{6}
\end{equation*}
$$

where

$$
\begin{gathered}
\overline{G_{\text {growth }}}\left(T, V_{p}\right)=\int_{0}^{\infty} V_{p}^{k} \frac{\partial\left[G\left(T, V_{p}\right) u_{d}\left(T, V_{p}\right)\right]}{\partial V_{p}} d V_{p} \\
\overline{Q_{\text {nucleation }}}\left(T, V_{p}\right)=\int_{0}^{\infty} V_{p}^{k} Q_{n u c}\left(T, V_{p}\right) d V_{p} \\
\overline{Q_{\text {aggregation }}}\left(T, V_{p}\right)=\overline{B_{\mathrm{agg}}}\left(T, V_{p}\right)-\overline{D_{\mathrm{agg}}}\left(T, V_{p}\right)
\end{gathered}
$$

The aggregation terms $\overline{B_{\mathrm{agg}}}\left(T, V_{p}\right)$ and $\overline{D_{\mathrm{agg}}}\left(T, V_{p}\right)$ are mathematically defined as

$$
\begin{gathered}
\overline{B_{\mathrm{agg}}}\left(T, V_{p}\right)=\frac{1}{2} \int_{0}^{\infty} V_{p}^{k} \int_{0}^{V_{p}} \beta\left(T, V_{p}-V_{p}^{\prime}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}-V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} d V_{p} \\
\overline{D_{\mathrm{agg}}}\left(T, V_{p}\right)=\int_{0}^{\infty} V_{p}^{k} u_{d}\left(T, V_{p}\right) \int_{0}^{\infty} \beta\left(T, V_{p}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} d V_{p} \\
\\
Q_{\text {breakage }}\left(T, V_{p}\right)=\overline{B_{\text {break }}}\left(T, V_{p}\right)-\overline{D_{\text {break }}}\left(T, V_{p}\right)
\end{gathered}
$$

whereas $\overline{B_{\text {break }}}\left(T, V_{p}\right)$ and $\overline{D_{\text {break }}}\left(T, V_{p}\right)$ are birth and death functions because of breakage term and are given by

$$
\begin{gathered}
\overline{B_{\text {break }}}\left(T, V_{p}\right)=\int_{0}^{\infty} V_{p}^{k} \int_{V_{p}}^{\infty} b\left(T, V_{p}, V_{p}^{\prime}\right) S\left(V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} d V_{p} \\
\overline{B_{\text {break }}}\left(T, V_{p}\right)=\int_{0}^{\infty} V_{p}^{k} S\left(V_{p}\right) u_{d}\left(T, V_{p}\right) d V_{p} \\
\overline{Q_{\text {dissolution }}}\left(T, V_{p}\right)=\frac{\dot{V}}{V_{c}} \int_{0}^{\infty} V_{p}^{k} h\left(V_{p}\right) u_{d}\left(T, V_{p}\right) d V_{p}
\end{gathered}
$$

Due to aggregation, the upper limit in the birth function is not infinity; therefore, we cannot apply quadrature method of moment for this integral. To apply the QMOM, we have to convert the upper limit to infinity. Here, we introduce a Heaviside step function $H\left(V_{p}-V_{p}^{\prime}\right)$ to solve the integral such that $H\left(V_{p}-V_{p}^{\prime}\right)=0$ when $V_{p}-V_{p}^{\prime}<0$ and $H\left(V_{p}-V_{p}^{\prime}\right)=1$ otherwise. As a result, we will find the limits of integration over $V_{p}^{\prime}$ from $\left(0, V_{p}\right)$ to $(0, \infty)$. Thus, by applying it to the birth function, we obtain the following equation:

$$
\begin{gather*}
\frac{1}{2} \int_{0}^{\infty} V_{p}^{k} d V_{p} \int_{0}^{\infty} H\left(V_{p}-V_{p}^{\prime}\right) \beta\left(T, V_{p}-V_{p}^{\prime}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}-V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} \\
=\frac{1}{2} \int_{0}^{\infty} u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} \int_{0}^{\infty}\left(u+V_{p}^{\prime}\right)^{k} \beta\left(T, u, V_{p}^{\prime}\right) u_{d}(T, u) d V_{p} \tag{7}
\end{gather*}
$$

On the right side of Equation (7), we have switched the order of integration and made the replacement $u=V_{p}-V_{p}^{\prime}$. Lastly, we have replaced $V_{p}$ for $u$ with no damage of generality and caught the necessary outcome for birth due to aggregation which is given by

$$
\overline{B_{\mathrm{agg}}}\left(T, V_{p}\right)=\frac{1}{2} \int_{0}^{\infty} u_{d}\left(T, V_{p}^{\prime}\right) \int_{0}^{\infty}\left(V_{p}+V_{p}^{\prime}\right) \beta\left(T, V_{p}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}\right) d V_{p} d V_{p}^{\prime}
$$

After substituting all of the above terms in Equation (6), we get the system of differential equations:

$$
\begin{align*}
\frac{d m_{k}(T)}{d T} & =\int_{0}^{\infty} k V_{p}^{k-1} G\left(T, V_{p}\right) u_{d}\left(T, V_{p}\right) d V_{p}+\int_{0}^{\infty} V_{p}^{k} Q_{n u c}\left(T, V_{p}\right) d V_{p} \\
& +\frac{1}{2} \int_{0}^{\infty} u_{d}\left(T, V_{p}^{\prime}\right) \int_{0}^{\infty}\left(V_{p}+V_{p}^{\prime}\right)^{k} \beta\left(T, V_{p}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}\right) d V_{p} d V_{p}^{\prime} \\
& -\int_{0}^{\infty} V_{p}^{k} u_{d}\left(T, V_{p}\right) \int_{0}^{\infty} \beta\left(T, V_{p}, V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} d V_{p}  \tag{8}\\
& +\int_{0}^{\infty} V_{p}^{k} \int_{V_{p}}^{\infty} b\left(T, V_{p}, V_{p}^{\prime}\right) S\left(V_{p}^{\prime}\right) u_{d}\left(T, V_{p}^{\prime}\right) d V_{p}^{\prime} d V_{p} \\
& -\int_{0}^{\infty} V_{p}^{k} S\left(V_{p}\right) u_{d}\left(T, V_{p}\right) d V_{p}+\frac{\dot{V}}{V_{c}} \int_{0}^{\infty} V_{p}^{k} h\left(V_{p}\right) u_{d}\left(T, V_{p}\right) d V_{p}
\end{align*}
$$

In addition, with solid phase, the liquid phase yields ordinary differential equation for the solute mass in the form:

$$
\begin{equation*}
\frac{d m(T)}{d T}=\dot{m_{\text {in }}}(T)-\dot{m}_{\text {out }}(T)-3 \sigma_{c} k_{v} \int_{0}^{\infty} V_{p}^{2} G\left(T, V_{p}\right) u_{d}\left(T, V_{p}\right) d V_{p} \tag{9}
\end{equation*}
$$

with $m(0)=m_{0}$ where $\sigma_{c}$ is the density of crystals and $k_{v}$ is a volume shape factor. $\dot{m}_{\text {in }}(T)-\dot{m_{\text {in }}}(T)-$ is the incoming mass flux from dissolution unit to crystallizer and outgoing mass flux from crystallizer to dissolution unit, respectively, which is mathematically defined by

$$
\begin{equation*}
m_{\mathrm{out}}(T)=\frac{m(T)}{m(T)+m_{\mathrm{solv}}(T)} \sigma_{\text {sol }}(T) \dot{V} \tag{10}
\end{equation*}
$$

where $m_{\text {solv }}(T)$ is the mass of solvent and $\sigma_{\text {sol }}(T)$ is the density of the solution. $T_{p}=\frac{V_{p}}{V} \geq 0$ is the residence time in the dissolution unit, where $V_{p}$ represents volume of the pipe.

Here, we will consider the Gaussian quadrature method to solve the complicated integral terms appearing in Equations (8) and (9). Consequently, a closed-form system of moments is found. Further, we have accurately and efficiently solved the closed-form system with an ODE solver. The approximation of definite integral with the help of quadrature rule is an important numerical aspect. For this purpose, first we calculate the function at definite points and then use the formula of weight function which gives approximation of the definite integral. To approximate a definite integral given in Equations (8) and (9), first we find the values of the function at a set of equidistant points. After evaluating, the weight function is multiplied to approximate the integrals. In this rule, there is no limitation of choosing abscissas and weights. This rule also works for the points which are not likewise spread out. Let us assume the integral of the formula $\int_{a}^{b} \psi\left(V_{p}\right) u_{d}\left(V_{p}\right) d V_{p}$. We can find the weights $w_{j}$ and abscissas $V_{k p_{i}}$ by approximating the definite integral as

$$
\begin{equation*}
\int_{a}^{b} \psi\left(V_{p}\right) u_{d}\left(V_{p}\right) d V_{p}=\sum_{j=1}^{N} w_{j} u_{d}\left(V_{p_{j}}\right) \tag{11}
\end{equation*}
$$

where provided it is exact and $u_{d}\left(V_{p}\right)$ is smooth function. A set of orthogonal polynomials is necessary for making certain $n^{\text {th }}$ order orthogonal polynomial and it should contain only one polynomial of order $j$ for $j=1,2,3, \ldots$. We can define the scalar product of the two functions $k\left(V_{p}\right)$ and $h\left(V_{p}\right)$ over a weight function $\psi\left(V_{p}\right)$ by

$$
\begin{equation*}
<h \backslash k>=\int_{a}^{b} \psi\left(V_{p}\right) h\left(V_{p}\right) k\left(V_{p}\right) d V_{p} \tag{12}
\end{equation*}
$$

If we find the zero scalar product of any two functions $h$ and $k$, then these functions are termed as orthogonal functions. It is also noted that supplementary information will be required for obtaining abscissas and weights if the classical weight function $\psi\left(V_{p}\right)$ is not provided. For this purpose, we have used the moment:

$$
\begin{equation*}
m_{i}(T)=\int_{0}^{\infty} V_{p}^{i} u_{d}\left(T, V_{p}\right) d V_{p} \approx \sum_{j=1}^{N} V_{p_{j}}^{j} w_{j} \tag{13}
\end{equation*}
$$

In the above equation, $u_{d}\left(T, V_{p}\right)$ is used as a weight function $\psi\left(V_{p}\right) . V_{p}^{i}$ given in Equation (13) denotes the polynomial $u_{d}\left(V_{p}\right)$ of $i^{\text {th }}$ order. To find $n$ abscissas weights, we need $2 n$ moments from $m_{0}$ to $m_{2 n-1}$. For $i \leq 2 n-1$ this approximation will be exact. For simplicity and accurate approximations, we set $n=3$. As a result, six-moment system for $m_{0}, \ldots \ldots, m_{5}$ is calculated. To discuss the procedure, we consider ODEs (8) and (9). Using Equation (13) in Equations (8) and (9), we obtain the following equations:

$$
\begin{align*}
\frac{d m_{k}(T)}{d T} & =k \sum_{i=1}^{N}\left(V_{p_{i}}\right)^{k-1} w_{i} G\left(T, V_{p_{i}}\right)+a_{n u c}^{(k)} \\
& +\frac{1}{2} \sum_{i=1}^{N} w_{i} \sum_{j=1}^{N}\left(V_{p_{i}}+V_{p_{j}}\right)^{k} \beta\left(T, V_{p_{i}}, V_{p_{j}}\right) w_{j} \\
& -\sum_{i=1}^{N}\left(V_{p_{i}}\right)^{k} w_{i} \sum_{j=1}^{N} \beta\left(T, V_{p_{i}}, V_{p_{j}}\right) w_{j}  \tag{14}\\
& +\sum_{i=1}^{N}\left(V_{p_{i}}\right)^{k} w_{i} \sum_{j=1}^{N} \beta\left(T, V_{p_{i}}, V_{p_{j}}\right) S\left(V_{p_{j}}\right) w_{j} \\
& +\dot{V} V_{c} \sum_{i=1}^{N} w_{i}\left(V_{p_{i}}\right)^{k} h\left(V_{p_{i}}\right) \quad k=0,1,2, \ldots \ldots
\end{align*}
$$

where $a_{n u c}^{(k)}=\int_{0}^{\infty} V_{p}{ }^{k} Q_{n u c} d V_{p}$ and

$$
\begin{equation*}
\frac{d m(T)}{d T}=\dot{m_{\mathrm{in}}}(T)-m_{\mathrm{out}}(T)-3 \sigma_{c} k_{v} \sum_{i}^{N} w_{i} V_{p}^{2} G\left(T, V_{p_{i}}\right) \tag{15}
\end{equation*}
$$

Our next step is computing the quadrature points $V_{p i}, V_{p j}^{\prime}$ and the quadrature weights $w_{i}$ and $w_{j}$. The quadrature points $V_{p i}, V_{p j}^{\prime}$ are obtained from the roots of orthogonal polynomials. The construction of orthogonal polynomials is described as follows:

$$
\begin{equation*}
p_{-1}=0, p_{0}=1, p_{j}=\left(V_{p}-\alpha_{j}\right) p_{j-1}-\beta_{j} p_{j-1} \tag{16}
\end{equation*}
$$

with

$$
\begin{gather*}
\alpha_{j}=\frac{\left\langle V_{p} p_{j-1} / p_{j-1}\right\rangle}{\left\langle p_{j-1} / p_{j-1}\right\rangle}, j=1,2, \ldots  \tag{17}\\
\beta_{j}=\frac{\left\langle p_{j-1} / p_{j-1}\right\rangle}{\left\langle p_{j-2} / p_{j-2}\right\rangle}, j=2,3, \ldots \tag{18}
\end{gather*}
$$

Since the function $u_{d}\left(T, V_{p}\right)$ is used as a weight function $\psi\left(V_{p}\right)$, so from Equation (12) we have

$$
<p_{j} / p_{j}>=\int_{a}^{b} u_{d}\left(T, V_{p}\right) p_{j}^{2} d V_{p}
$$

Using all of the above definitions, the orthogonal polynomials of any order can be obtained. Our first step is to find the roots of the $n^{\text {th }}$ order polynomial. The quadrature points $V_{p}$ are then obtained from these roots. To explain the procedure of deriving these orthogonal polynomials, we have calculated $p_{1}\left(V_{p}\right), p_{2}\left(V_{p}\right), p_{3}\left(V_{p}\right), p_{1}\left(V_{p}\right)$ as

$$
p_{1}\left(V_{p}\right)=\left(V_{p}-\alpha_{1}\right) p_{0}=\left(V_{p}-\alpha_{1}\right)
$$

First, $\alpha_{1}$ will be calculated, which is given by

$$
\alpha_{1}=\frac{<V_{p} p_{0} / p_{0}>}{\left\langle p_{0} / p_{0}>\right.}=\frac{\int_{0}^{\infty} V_{p} u_{d}\left(T, V_{p}\right) p_{0}^{2} d V_{p}}{\int_{0}^{\infty} u_{d}\left(T, V_{p}\right) p_{0}^{2} d V_{p}}=\frac{m_{1}(T)}{m_{0}(T)}
$$

so

$$
\begin{equation*}
p_{1}\left(V_{p}\right)=V_{p}-\frac{m_{1}}{m_{0}} \tag{19}
\end{equation*}
$$

Now

$$
\begin{equation*}
p_{2}\left(V_{p}\right)=\left(V_{p}-\alpha_{2}\right) p_{1}-\beta_{2} p_{1} \tag{20}
\end{equation*}
$$

Again from Equations (17) and (18) we have

$$
\begin{equation*}
\alpha_{2}=\frac{\left\langle V_{p} p_{1} / p_{1}\right\rangle}{\left\langle p_{1} / p_{1}\right\rangle}=\frac{\int_{0}^{\infty} V_{p} u_{d}\left(T, V_{p}\right) p_{1}^{2} d V_{p}}{\int_{0}^{\infty} u_{d}\left(T, V_{p}\right) p_{1}^{2} d V_{p}}=\frac{\int_{0}^{\infty} V_{p} u_{d}\left(T, V_{p}\right)\left(V_{p}-\frac{m_{1}}{m_{0}}\right)^{2} d V_{p}}{\int_{0}^{\infty} u_{d}\left(T, V_{p}\right)\left(V_{p}-\frac{m_{1}}{m_{0}}\right)^{2} d V_{p}}=\frac{m_{3} m_{0}^{2}-2 m_{0} m_{1} m_{2}+m_{1}^{3}}{m_{2} m_{0}^{2}-m_{0} m_{1}^{2}} \tag{21}
\end{equation*}
$$

and

$$
\begin{equation*}
\beta_{2}=\frac{<p_{1} / p_{1}>}{<p_{0} / p_{0}>}=\frac{\int_{0}^{\infty} V_{p} u_{d}\left(T, V_{p}\right)\left(V_{p}-\frac{m_{1}}{m_{0}}\right)^{2} d V_{p}}{\int_{0}^{\infty} u_{d}\left(T, V_{p}\right) d V_{p}}=\frac{m_{2} m_{0}-m_{1}^{2}}{m_{0}^{2}} \tag{22}
\end{equation*}
$$

so from Equation (20) we have

$$
\begin{equation*}
p_{2}\left(V_{p}\right)=\frac{V_{p}^{2}\left(m_{0} m_{2}-m_{1}^{2}\right)+V_{p}\left(m_{1} m_{2}-m_{0} m_{3}\right)+m_{1} m_{3}-m_{2}^{2}}{m_{0} m_{2}-m_{1}^{2}} \tag{23}
\end{equation*}
$$

Proceeding in a similar way, we can calculate the polynomial of higher order. The third-order polynomial $p_{3}\left(V_{p}\right)$ is given by the following equation:

$$
\begin{align*}
p_{3}\left(V_{p}\right) & =V_{p}^{3}+\frac{\left(m_{2} m_{4} m_{1}-m_{0} m_{4} m_{3}+m_{2} m_{0} m_{5}+m_{3}^{2} m_{1}-m_{5} m_{1}^{2}-m_{2}^{2} m_{3}\right) V_{p}^{2}}{m_{2}^{3}-m_{2} m_{4} m_{0}-2 m_{2} m_{3} m_{1}+m_{3}^{2} m_{0}+m_{4} m_{1}^{2}}  \tag{24}\\
& +\frac{\left(m_{2} m_{5} m_{1}+m_{0} m_{4}^{2}-m_{0} m_{5} m_{3}-m_{4} m_{3} m_{1}-m_{2}^{2} m_{4}+m_{3}^{2} m_{2}\right) V_{p}}{m_{2}^{3}-m_{2} m_{4} m_{0}-2 m_{2} m_{3} m_{1}+m_{3}^{2} m_{0}+m_{4} m_{1}^{2}}+\frac{\left.2 m_{2} m_{4} m_{3}-m_{2}^{2} m_{5}-m_{3}^{3}-m_{4}^{2} m_{1}+m_{5} m_{3} m_{1}\right)}{m_{2}^{3}-m_{2} m_{4} m_{0}-2 m_{2} m_{3} m_{1}+m_{3}^{2} m_{0}+m_{4} m_{1}^{2}}
\end{align*}
$$

The roots of the selected polynomial will give us the abscissas $V_{p}$. Next, the weights $w_{i}$ will be calculated. According to Press et al. [15], the expression for the weight function is given by

$$
\begin{equation*}
w_{i}=\frac{\left\langle p_{N-1} / p_{N-1}\right\rangle}{p_{N-1}\left(x_{j}\right) p_{N}^{\prime}\left(x_{j}\right)} \quad i=1,2, \ldots \ldots \ldots . N \tag{25}
\end{equation*}
$$

where $N$ is the order of the selected polynomial. At last, the resulting system of ODEs is then solved by any standard ODE solver in MatLab.

## 3. Results

Test Problem 1: Aggregation with Fines Dissolution
Here, the proposed scheme is analyzed for aggregation with fines dissolution (see Figure 1) problem encountered in several particulate methods (i.e., fluidized beds, formation of rain droplets, and manufacture of dry powders). The effects of further procedures, such as breakage, growth, and nucleation, are negligible. During the aggregation process, the total mass of particles $m_{1}$ is conserved and the amount of particles $m_{0}$ reduces during the processing time. The aggregation kernel is held to be constant and is defined as $\beta\left(V_{p}, V_{p}^{\prime}\right)=\beta_{0}$, where $\beta_{0}=1$. The exponential initial particle size distribution is given by

$$
\begin{equation*}
u_{d}\left(0, V_{p}\right)=\frac{N_{0}}{V_{P_{0}}} \exp \left(-V_{p} / V_{P_{0}}\right) \tag{26}
\end{equation*}
$$

where $N_{0}=1$ and $V_{p 0}=1$. The dissolution term $h\left(V_{p}\right)$ explains the dissolution of particles below certain critical size, that is, $2 \times 10^{-4} \mathrm{~m}^{3}$. The analytical solution in terms of the number density $u_{d}\left(T, V_{p}\right)$ is given by $\operatorname{Scott}$ [16]:

$$
\begin{equation*}
u_{d}\left(T, V_{p}\right)=\frac{4 N_{0}}{V_{P_{0}}(\tau+2)^{2}} \exp \left(-2 V_{p}^{\prime} / \tau+2\right) \tag{27}
\end{equation*}
$$

where $\tau=N_{0} \beta_{0} t$ and $V_{p}^{\prime}=V / V_{p 0}$. The plot in Figure 2 shows normalized moments. The outcomes of our QMOM are in decent agreement with analytical outcomes. It is also observed from Figure 2 that during the aggregation process, the number of particles $m_{0}(T)$ decreases while the volume of the particles $m_{1}(T)$ remains constant.


Figure 1. Single batch setup process with fines dissolution.


Figure 2. Aggregation with fines dissolution.

Test Problem 2: Aggregation and Breakage with Fines Dissolution
In this problem, we take a batch crystallizer in which aggregation and breakage are the main occurrences and which is connected with a fines dissolver. The growth and nucleation terms are neglected in this process. The initial distribution is given by

$$
\begin{equation*}
u_{d}\left(0, V_{p}\right)=M_{0} \cdot \frac{M_{0}}{M_{1}} \exp \left(-\frac{M_{0}}{M_{1}} V_{p}\right) \tag{28}
\end{equation*}
$$

where, $M_{0}=\frac{2 N_{0}}{2+\beta_{0} N_{0} t}$ and $M_{1}=N_{0} V_{p 0}\left[1-\frac{2 G_{0}}{\beta_{0} N_{0} V_{p 0}} \ln \left(\frac{2}{2+\beta_{0} N_{0} t}\right)\right]$ represent the zero and first moments, respectively. A constant aggregation term, $\beta\left(V_{p}, V_{p}^{\prime}\right)=\beta_{0}=1$, a breakage kernel $b\left(V_{p}, V_{p}^{\prime}\right)=2 / V_{p,}^{\prime}$, and uniform daughter distribution $S\left(V_{p}\right)=V_{p}$ are taken. The analytical solution is given by Patel [17]:

$$
\begin{equation*}
u_{d}\left(T, V_{p}\right)=\frac{M_{0}^{2}}{M_{1}} \exp \left(-\frac{M_{0}}{M_{1}} V_{p}\right) \tag{29}
\end{equation*}
$$

The numerical results are displayed in Figure 3. The moments of the numerical system are in good agreement with those taken from the analytical solution. It is also observed from Figure 3 that during the aggregation and breakage process, the number of particles $m_{0}(T)$ decreases while the volume of the particles $m_{1}(T)$ remains constant.


Figure 3. Aggregation and breakage with fines dissolution.

## 4. Conclusions

The moment-generating function was used to convert the governing partial differential equation into a system of ordinary differential equations. The mathematical term for fines dissolution was incorporated in the model for improving the quality of the product. The Gaussian quadrature method was implemented to solve the complicated integrals in this research. An orthogonal polynomial of degree three, which utilizes the first six moments, was used for better accuracy of the proposed scheme. To check the significance of the scheme, two case studies were discussed. The results of the proposed scheme are in perfect agreement with the available analytical results. No dissipation was observed in the results. This work is extendable for batch preferential crystallization models with fines dissolution.

Furthermore, the developed scheme could be applicable to solve multidimensional batch crystallization models with fines dissolution.

Author Contributions: Conceptualization: S.M. and I.A.; Methodology: S.M.; Software: I.A. and M.S.; Validation: S.M. and I.A.;Formal Analysis: S.M.; Investigation: S.M.; Writing-Original Draft Preparation: S.M.; Writing-Review \& Editing: S.M., M.S., and I.A.
Funding: Safyan Mukhtar is thankful to the Deanship of Scientific Research, King Faisal University, for research grant through the Nasher track (186122).
Conflicts of Interest: The authors declare no conflict of interest.

## References

1. Hulburt, H.M.; Katz, S. Some problems in particle technology. Chem. Eng. Sci. 1964, 19, 555-574. [CrossRef]
2. Randolph, A.D.; Larson, M.A. Theory of Particulate Processes, 2nd ed.; Academic Press: Cambridge, MA, USA, 1988.
3. Barrett, J.C.; Jheeta, J.S. Improving the accuracy of the moments method for solving the aerosol general dynamic equation. J. Aerosol Sci. 1996, 27, 1135-1142. [CrossRef]
4. Fan, R.; Marchisio, D.L.; Fox, R.O. Application of the direct quadrature method of moments to polydisperse gas-solid fluidized beds. J. Powder Technol. 2004, 139, 7-20. [CrossRef]
5. Gimbbun, J.; Nagy, Z.K.; Rielly, C.D. Simultaneous quadrature method of moments for the solution of population balance equations using a differential algebraic framework. Ind. Chem. Eng. 2009, 48, 7798-7812. [CrossRef]
6. Gunawan, R.; Fusman, I.; Braatz, R.D. High resolution algorithms for multidimensional population balance equations. AICHE J. 2004, 50, 2738-2749. [CrossRef]
7. Kumar, S.; Ramkrishna, D. On the solution of population balance equations by discretization-I. A fixed pivot technique. Chem. Eng. Sci. 1996, 51, 1311-1332. [CrossRef]
8. Lim, Y.I.; Lann, J.-M.L.; Meyer, L.M.; Joulia, L.; Lee, G.; Yoon, E.S. On the solution of population balance equation (PBE) with accurate front tracking method in practical crystallization processes. Chem. Eng. Sci. 2002, 57, 3715-3732. [CrossRef]
9. Madras, G.; McCoy, B.J. Reversible crystal growth-dissolution and aggregation breakage: Numerical and moment solutions for population balance equations. J. Powder Technol. 2004, 143, 297-307. [CrossRef]
10. Marchisio, D.L.; Vigil, R.D.; Fox, R.O. Quadrature method of moments for aggregation-breakage processes. J. Colloid Interface Sci. 2003, 258, 322-334. [CrossRef]
11. Gahn, C.; Mersmann, A. Brittle fracture in crystallization processes Part A. Attrition and abrasion of brittle solids. Chem. Eng. Sci. 1999, 54, 1273-1282. [CrossRef]
12. McGraw, R. Description of aerosol dynamics by the quadrature method of moments. Aerosol Sci. Tech. 1997, 27, 255-265. [CrossRef]
13. Qamar, S.; Mukhtar, S.; Seidel-Morgenstern, A.; Elsner, M.P. An efficient numerical technique for solving one-dimensional batch crystallization models with size-dependent growth rates. Chem. Eng. Sci. 2009, 64, 3659-3667. [CrossRef]
14. Mukhtar, S.; Hussain, I.; Ali, A. Quadrature method of moments for solving volume-based population balance models. World Appl. Sci. J. 2012, 20, 1574-1583.
15. Press, W.H.; Teukolsky, S.A.; Vetterling, W.T.; Flannery, B.P. Numerical Recipes: The Art of Scientific Computing, 3rd ed.; Cambridge University Press: Cambridge, UK, 2007.
16. Scott, W.T. Analytic studies of cloud droplet coalescence I. J. Atmos. Sci. 1968, 25, 54-65. [CrossRef]
17. Patel, D.P.; Andrews, J.R.G. An analytical solution to continuous population balance model describing coalescence and breakage. J. Chem. Eng. Sci. 1998, 53, 599-601. [CrossRef]
