

Finding the Signal In the Noise

Determining North America's best path forward for sustainable energy

Canadian Journal of Chemical Engineering Lectureship Award Series

jfr photography



Thomas A. Adams II

Associate Professor, PhD, P.Eng

McMaster University

Department of Chemical Engineering

McMaster Advanced Control Consortium

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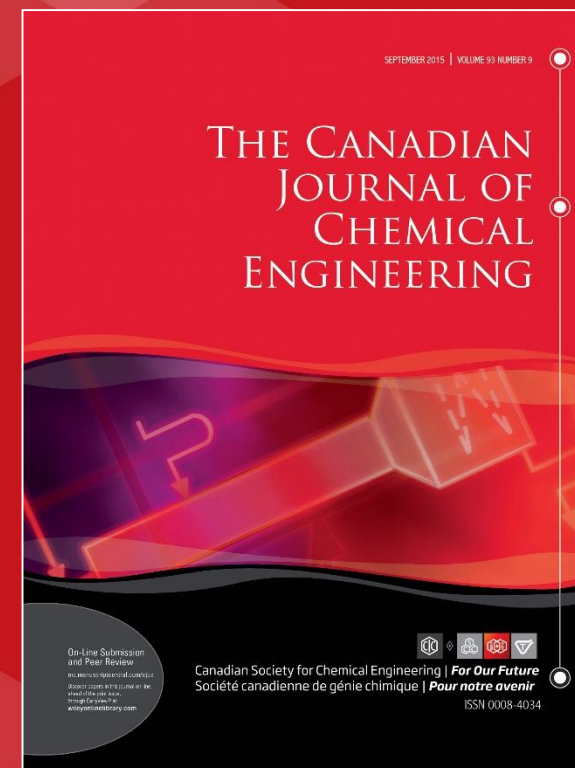
Thank you for your support!

Presenting results from the paper:

Nease J, Adams TA II. Life Cycle Analyses of Bulk-Scale Solid Oxide Fuel Cell Power Plants and Comparisons to the Natural Gas Combined Cycle.

Canadian J Chem Eng, 93:1349-1363 (2015).

(and others)



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- Links to articles cited in the study
- Links to data sets and simulations used in cited studies



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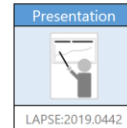
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Finding the Signal in the Noise: Determining North America's best path forward for sustainable energy

Thomas A Adams II

March 31, 2019



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Student Contribution Acknowledgements



Jake Nease

Professor at McMaster
University
(Former PhD Student)



Leila Hoseinzade

Engineer at
ArcelorMittal Dofasco
(Former PhD Student)



Pranav Madabhushi

PhD Candidate



Ikenna Okeke

PhD Candidate

Triple Bottom Line of Sustainability

Economical

- Capital
- Operating
- Supply Chain & Materials
- Job Creation / Losses
- Profitability
- Loans/Financing
- Stockholders
- Uncertainty and Risk

Environmental

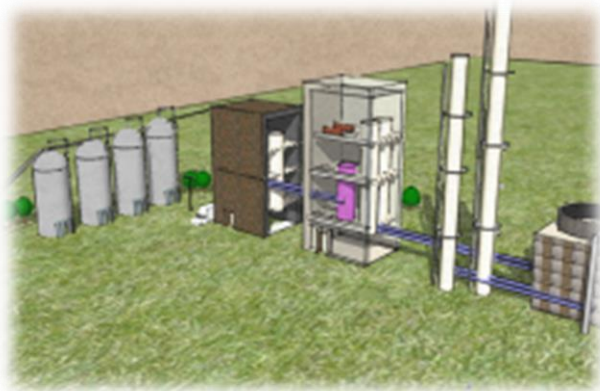
- Greenhouse Gases
- Particulates
- Deforestation
- Land Use / Transformation
- Resource Depletion
- Water Consumption
- Toxicity
- Wildlife Impact
- Noise

Societal

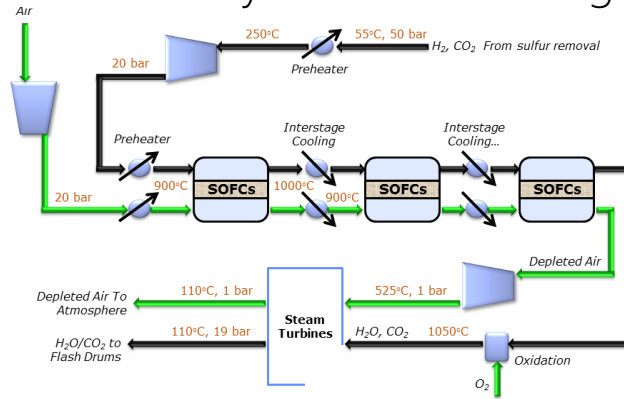
- Public Acceptance
- NIMBYs
- BANANAs
- Health Impacts
- Public/Employee Safety
- Accidents
- Public Policy
- Electoral Politics

Big Picture – Adams Group Research Methods

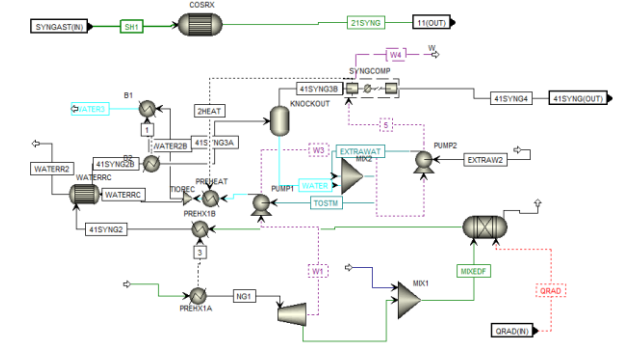
Unit Operation Design



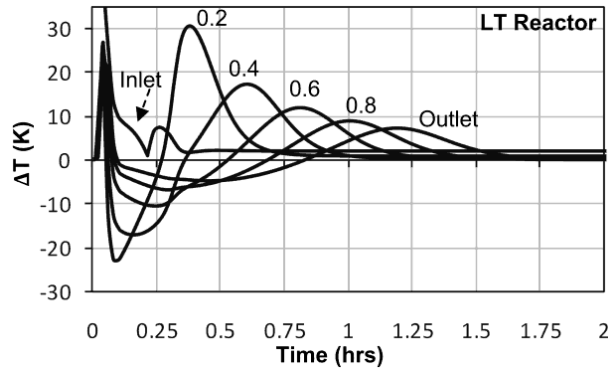
Process Synthesis and Design



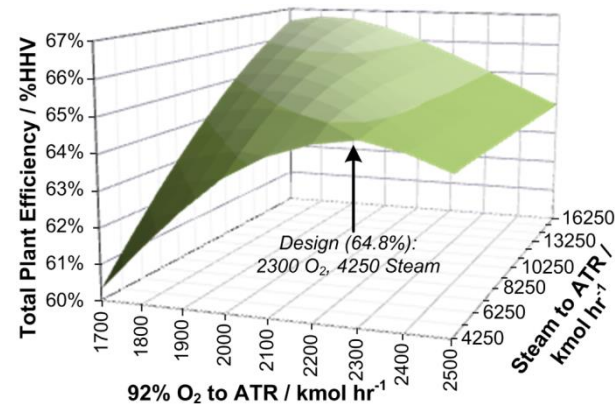
Process Modeling and Simulations



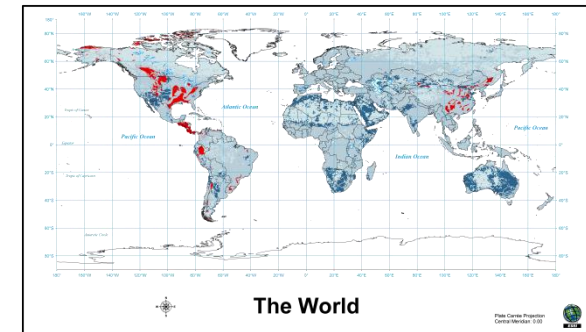
Process Dynamics



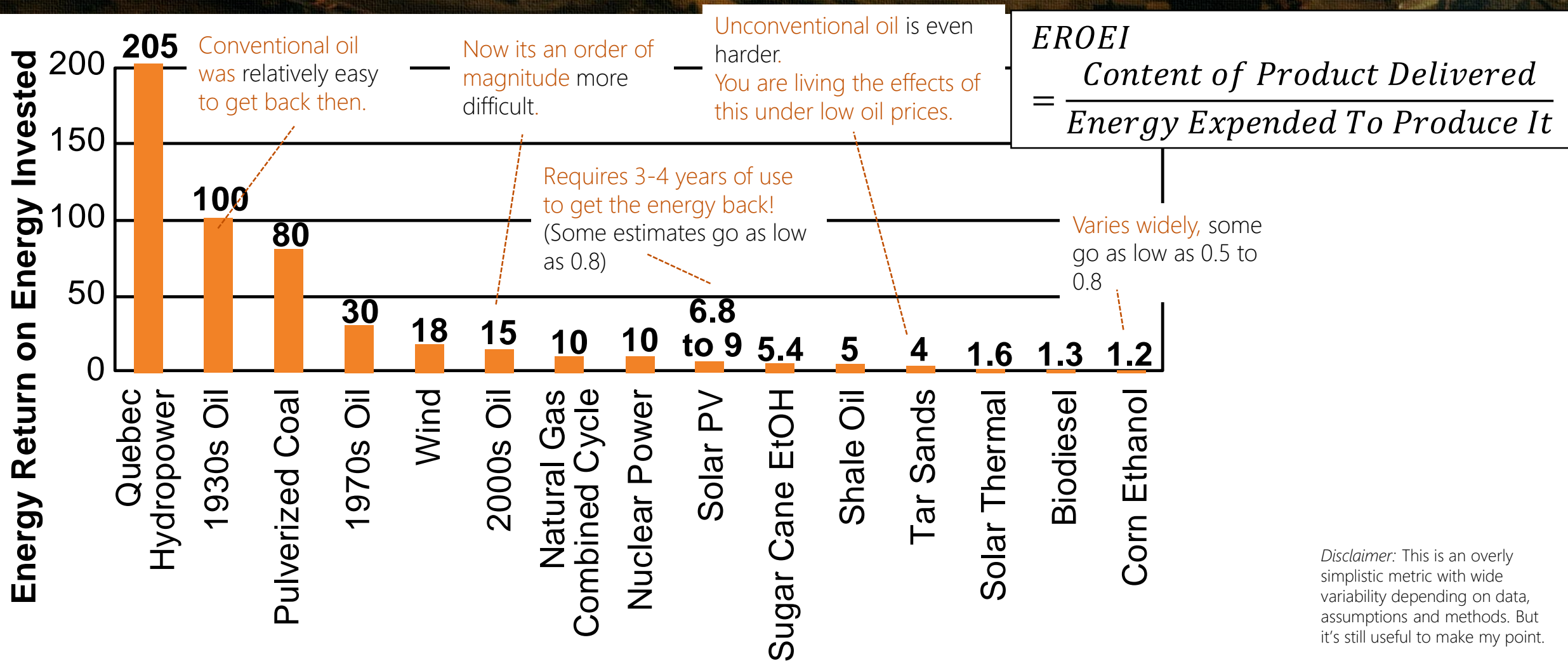
Process Optimization



Economics, Policy, and Environment (LCA)



Energy Return on Energy Invested (EROEI)



Disclaimer: This is an overly simplistic metric with wide variability depending on data, assumptions and methods. But it's still useful to make my point.

Scale and Why It Matters

- At \$50/tonne CO₂ emission tax (Canada Federal 2022 Minimum)
 - Global CO₂ Emissions: 36 billion tonne / yr
 - Global Tax Value: \$1.8 trillion / year (2.4% of World GDP)
 - Canada's GDP: \$1.5 trillion / year
- This is how the three tiers are linked in practice for Canada
 - (For climate change at least)
- Key Tools for Chemical Engineers:
 - Techno-economic analysis (TEA)
 - Life cycle analysis (LCA)

Big Picture Motivation

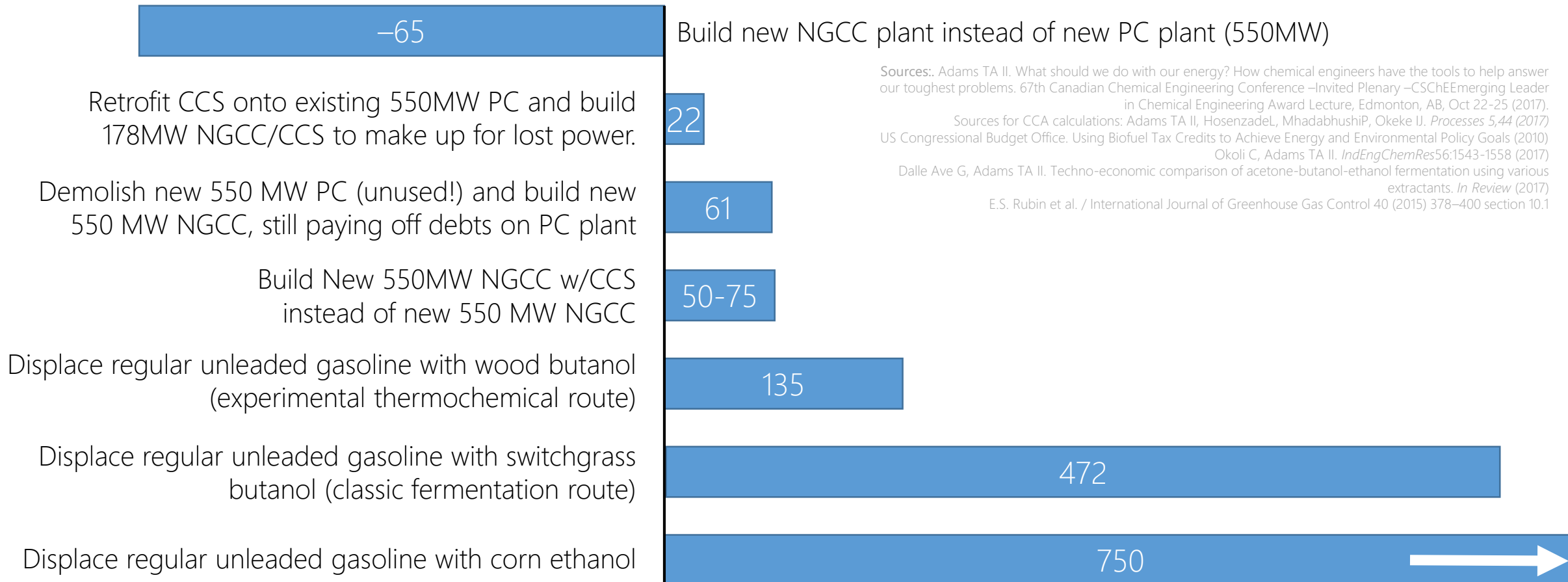
- We have **so many technology ideas** for reducing greenhouse emissions.
- Which should we **focus** on now?
- Where should our **money be invested**?
- **What should we do first**, and then next?

Cost of CO₂ Avoided: Where do we invest \$\$\$?

$$CCA = \frac{\text{Cost of Option 2} - \text{Cost of Status Quo}}{\text{GHG Emissions of Status Quo} - \text{GHG Emissions of Option 2}}$$

- Both should yield same product/service
- Use Life Cycle emissions

CCA (in 2016\$US per tonne of CO₂ equivalents)



Sources: Adams TA II. What should we do with our energy? How chemical engineers have the tools to help answer our toughest problems. 67th Canadian Chemical Engineering Conference –Invited Plenary –CSChEEmerging Leader in Chemical Engineering Award Lecture, Edmonton, AB, Oct 22-25 (2017).

Sources for CCA calculations: Adams TA II, HosenzadeL, MhadabhushiP, Okeke J. *Processes* 5,44 (2017)
US Congressional Budget Office. Using Biofuel Tax Credits to Achieve Energy and Environmental Policy Goals (2010)
Okoli C, Adams TA II. *IndEngChemRes*56:1543-1558 (2017)

Dalle Ave G, Adams TA II. Techno-economic comparison of acetone-butanol-ethanol fermentation using various extractants. *In Review* (2017)

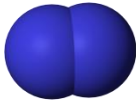
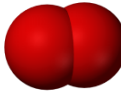
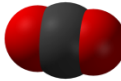

E.S. Rubin et al. / *International Journal of Greenhouse Gas Control* 40 (2015) 378–400 section 10.1

Fundamental Problem of CO₂ Capture and Sequestration

- **Fundamental problem:** separation of CO₂ and N₂ in flue gases:
 - We need to go from **dilute to high purity**

- We need to go from **low pressure to high pressure**
- And there's **an awful lot** of it (~7 million ton/yr per coal power plant).

TYPICAL COAL POWER FLUE EXHAUST, 1 BAR

	Mol %	Kinetic Diameter (Images to Scale)
N ₂ (&Ar)	68%	 3.6 Å
O ₂	2%	 3.45 Å
CO ₂	13%	 3.30 Å
H ₂ O	17%	 2.7 Å



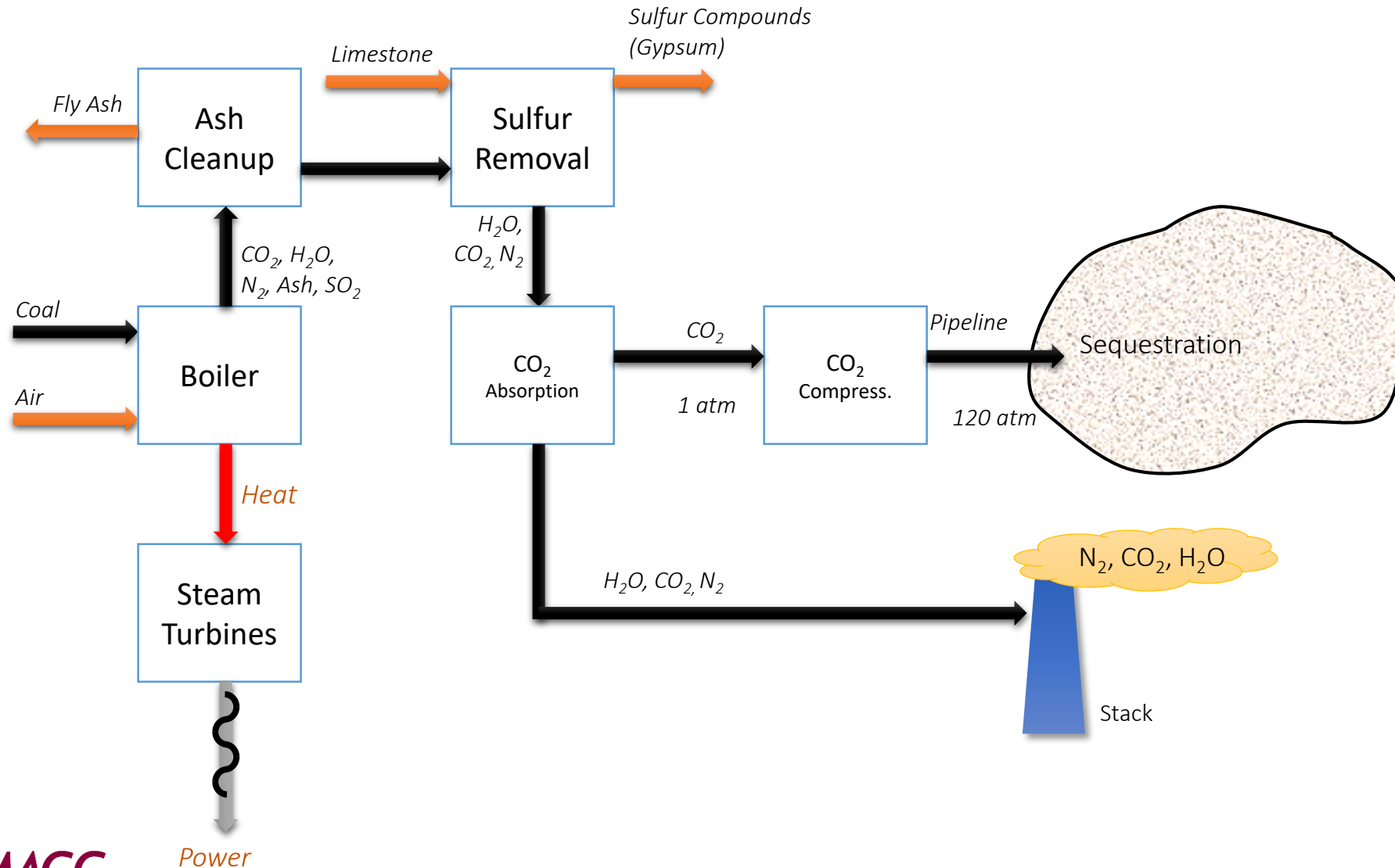
CO₂ PIPELINE LIMITS, 120 BAR

	Kinder Morgan	Sleipner
N ₂ (&Ar)	<4%	3-5%
O ₂	<50ppm	<50ppm
CO ₂	>95%	93-96%
H ₂ O	<690ppm	<Saturated

Sources: NETL 2007 - Bituminous Baseline Report (see required reading). Adams & Barton, AIChE J (2010) deVisser E., et al. Dynamis CO2 quality recommendations. Int. J. Greenhouse Gas Cont. 2008, 2, 478-484 Molecule Images from chemistry.about.com. Sizes from Angew. Chem. Int. Ed. 2010, 49, 6058 - 6082.

Post-Combustion Solvent-Based Capture

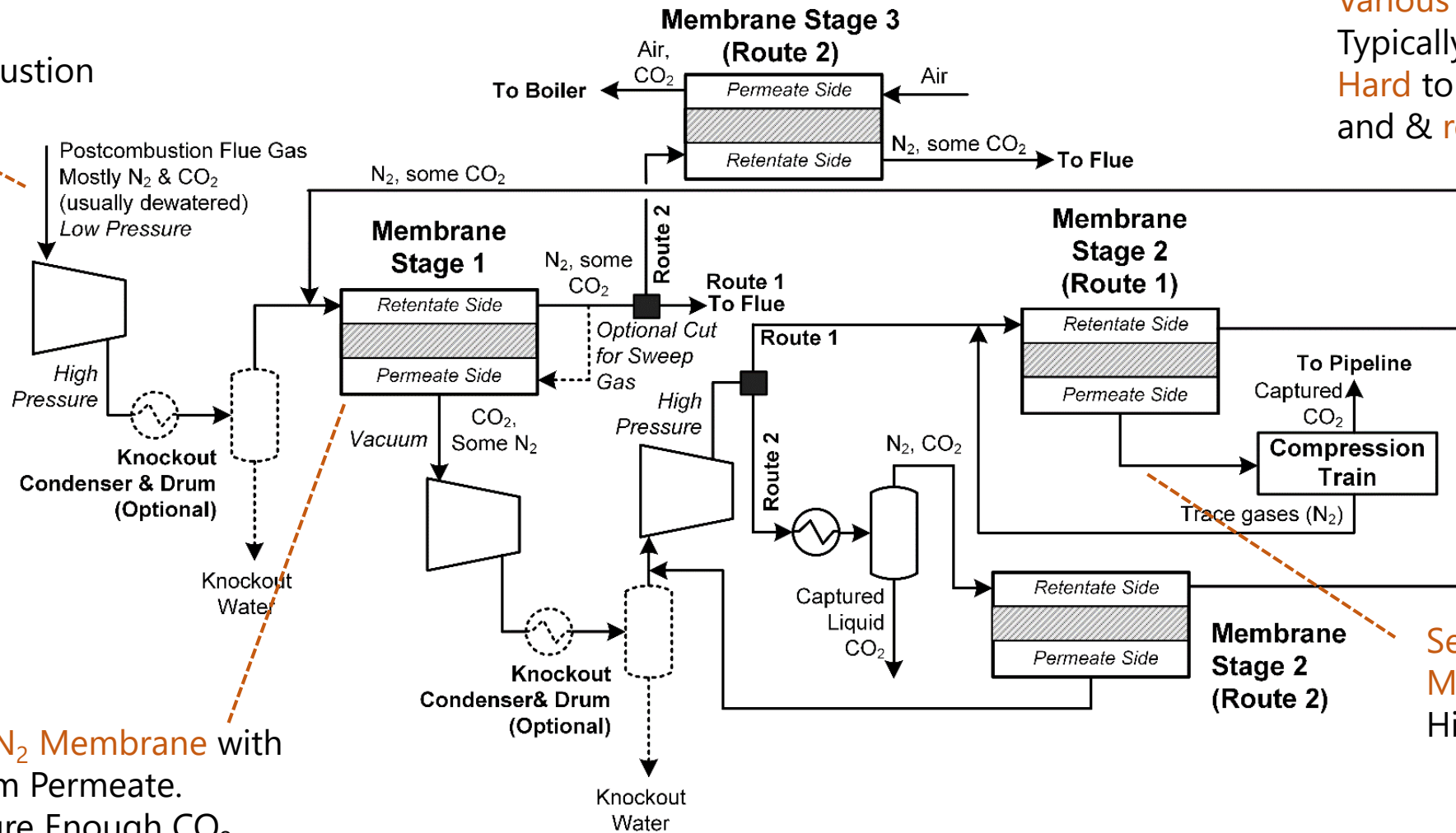
Pulverized Coal Example



Post-Combustion Membrane-Based Capture

Flue Gas from Upstream Combustion

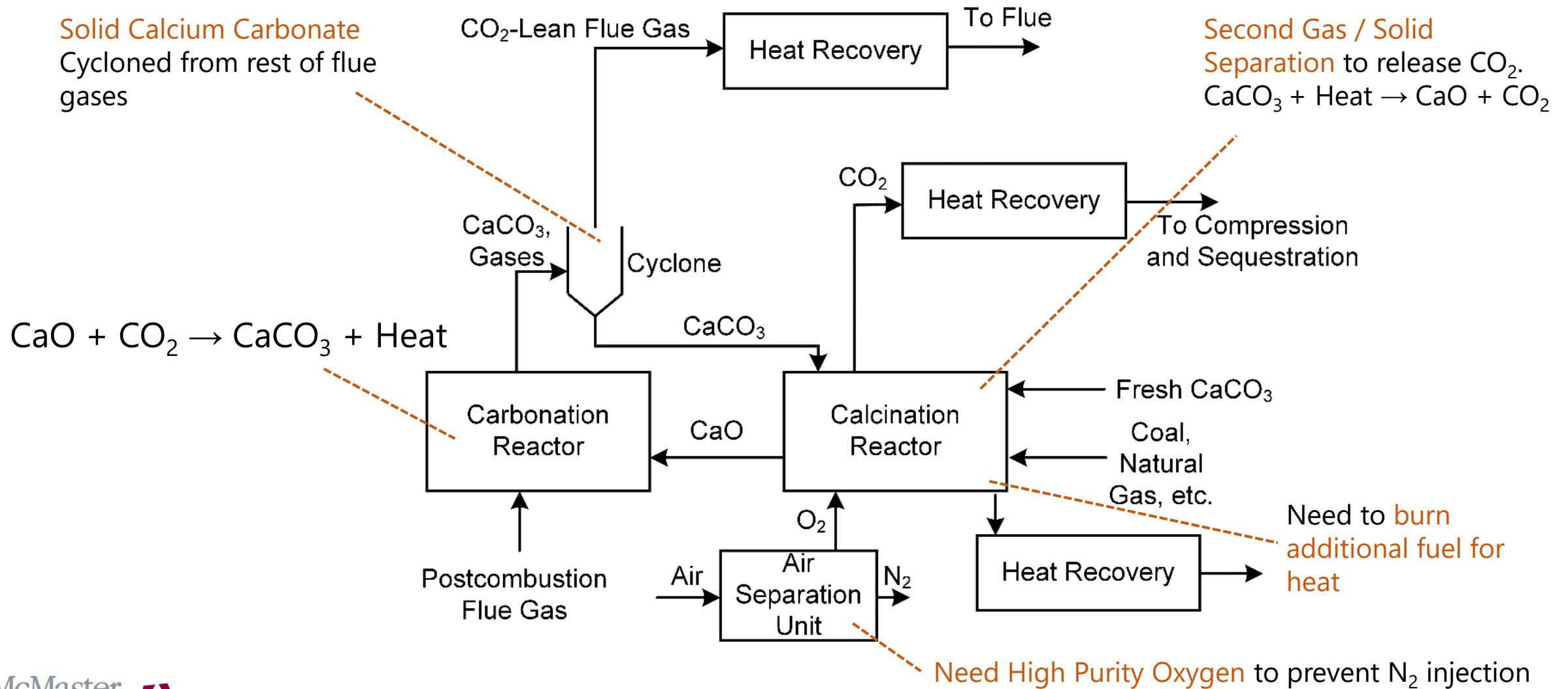
Various configurations
Typically 2 or 3 stages
Hard to get both purity and recovery



CO₂ / N₂ Membrane with Vacuum Permeate.
Not Pure Enough CO₂

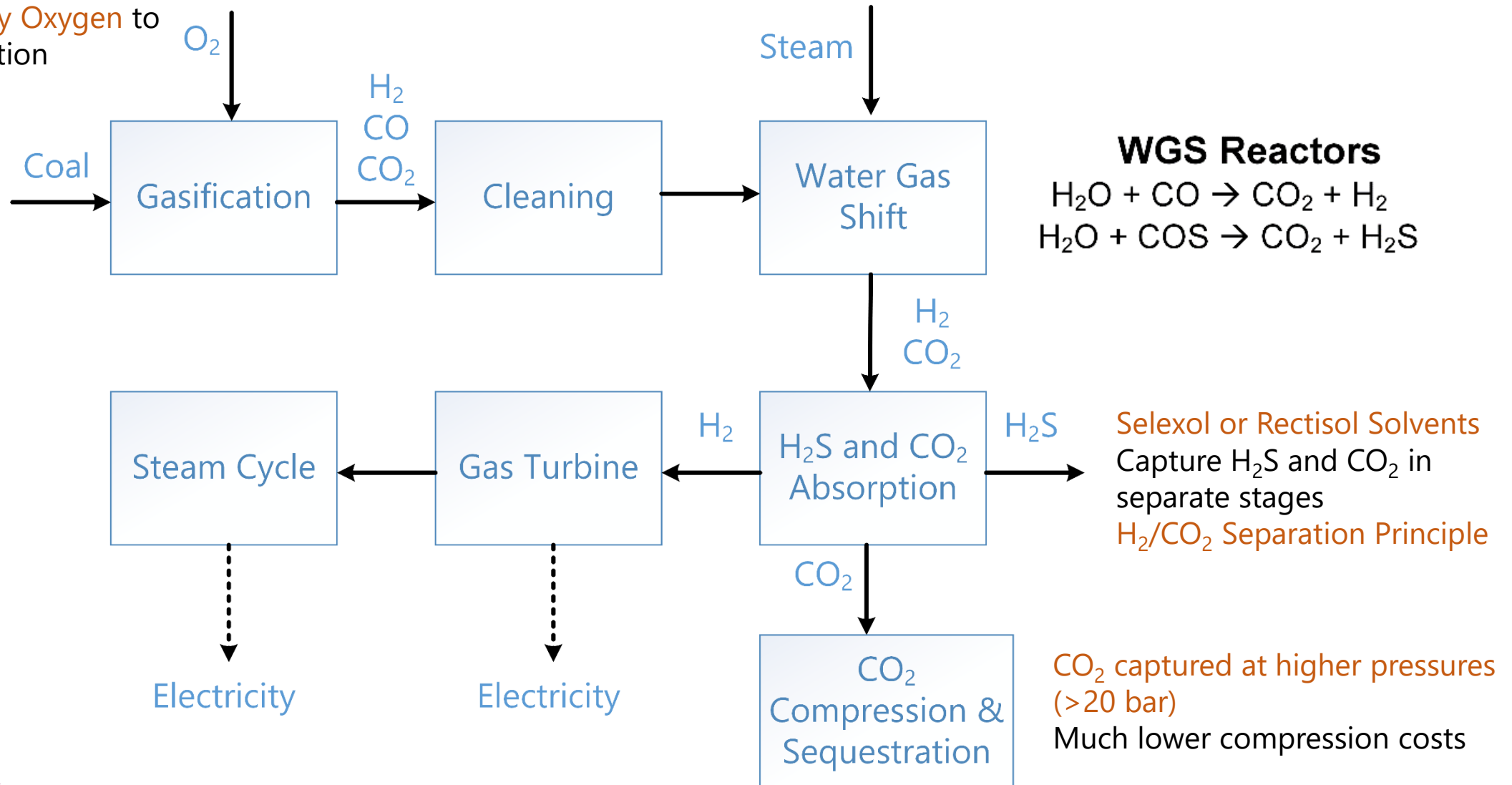
Second CO₂ / N₂ Membrane
Higher Purity CO₂

Post-Combustion Solid-Based Capture

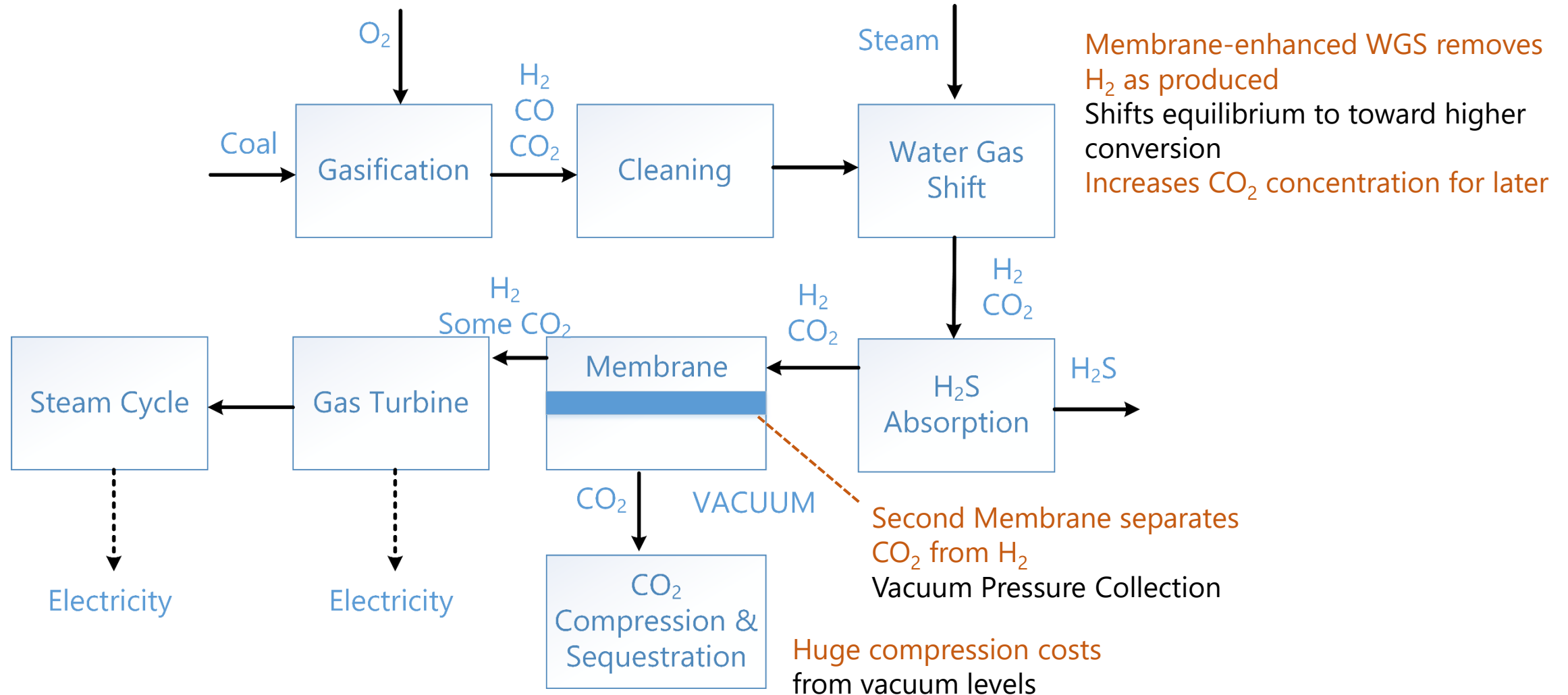


Pre-Combustion Solvent-Based Capture (IGCC)

Need High Purity Oxygen to prevent N₂ injection



Pre-Combustion Membrane-Based Capture



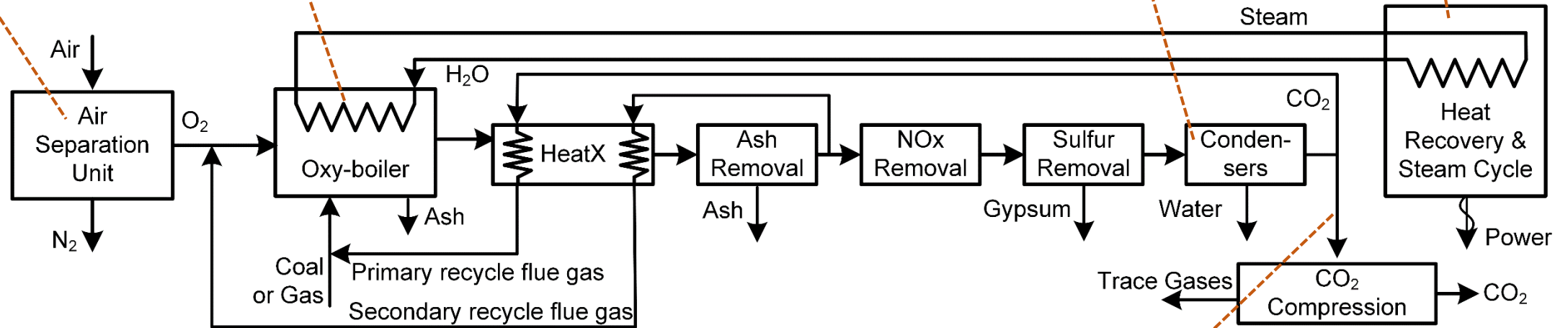
Oxyfuel Combustion

Fuel combusted in N₂-free flame
Diluted with CO₂ for thermal management

CO₂/H₂O Separation
via water condensation

Power Produced through
Steam Cycles

Very Large ASU



CO₂ captured at
atmospheric pressure

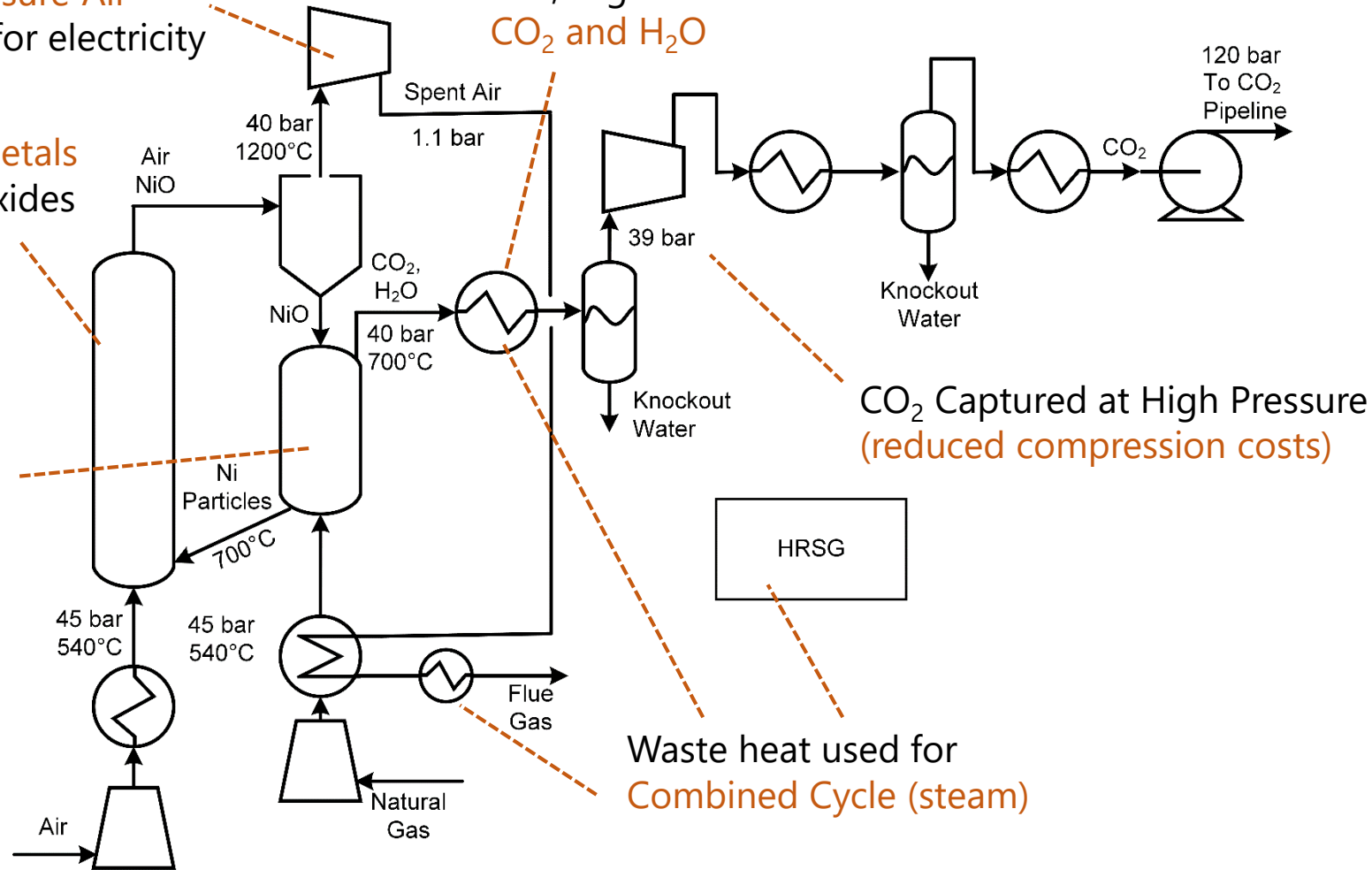
Chemical Looping Combustion

Hot, High Pressure Air
Spins turbine for electricity

Air reacts with reduced metals
Creates heat and metal oxides
 $O_2 + Me \rightarrow MeO + Heat$

Fuel combusts using
metal oxides instead of air
 $MeO + CH_4 + Heat \rightarrow H_2O + CO_2 + Me$

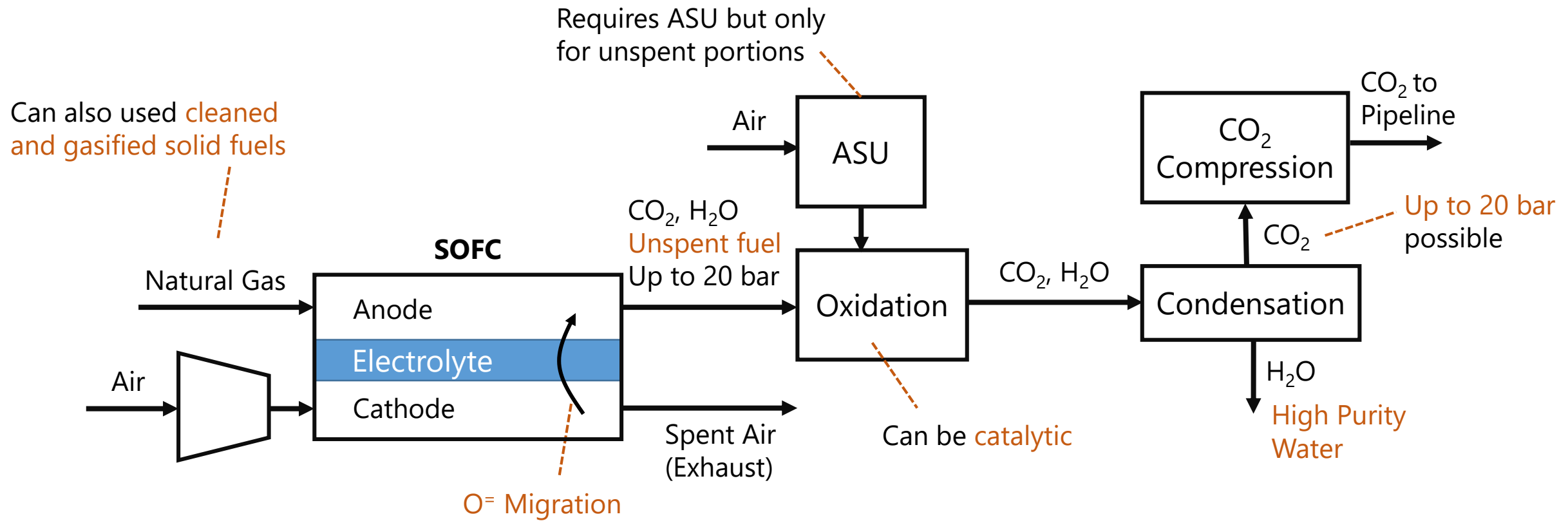
Hot, High Pressure
 CO_2 and H_2O



CO_2 Captured at High Pressure
(reduced compression costs)

Waste heat used for
Combined Cycle (steam)

Solid Oxide Fuel Cell (SOFC) Process



Recap

Type	Separation Problem	ASU Requirements	CO ₂ Capture Pressure	Example Applications
Solvent-based Post-Combustion	CO ₂ /N ₂	—	1 bar	Pulverized Coal, NGCC
Membrane-Based Post-Combustion	CO ₂ /N ₂	—	Vacuum	Pulverized Coal, NGCC
Solid-Based Post-Combustion	CO ₂ /N ₂	Low	1 bar	Pulverized Coal, NGCC
Solvent-Based Pre-Combustion	CO ₂ /H ₂	Medium	10-50 bar	IGCC, pre-reforming NGCC
Membrane-Based Pre-Combustion	CO ₂ /H ₂	Medium	Vacuum	IGCC, pre-reforming NGCC
Oxyfuels	CO ₂ /H ₂ O	High	1 bar	Gasified Coal/Nat Gas
Chemical Looping	CO ₂ /H ₂ O	—	10-50 bar	Gasified Coal/Nat Gas
Solid Oxide Fuel Cells	CO ₂ /H ₂ O	Low	1-20 bar	Gasified Coal/Nat Gas

Key Problems

- No systematic comparison between processes
- Everyone claims their own process is the best when compared against some other
- Wide variation in assumptions, strategies and ideas.

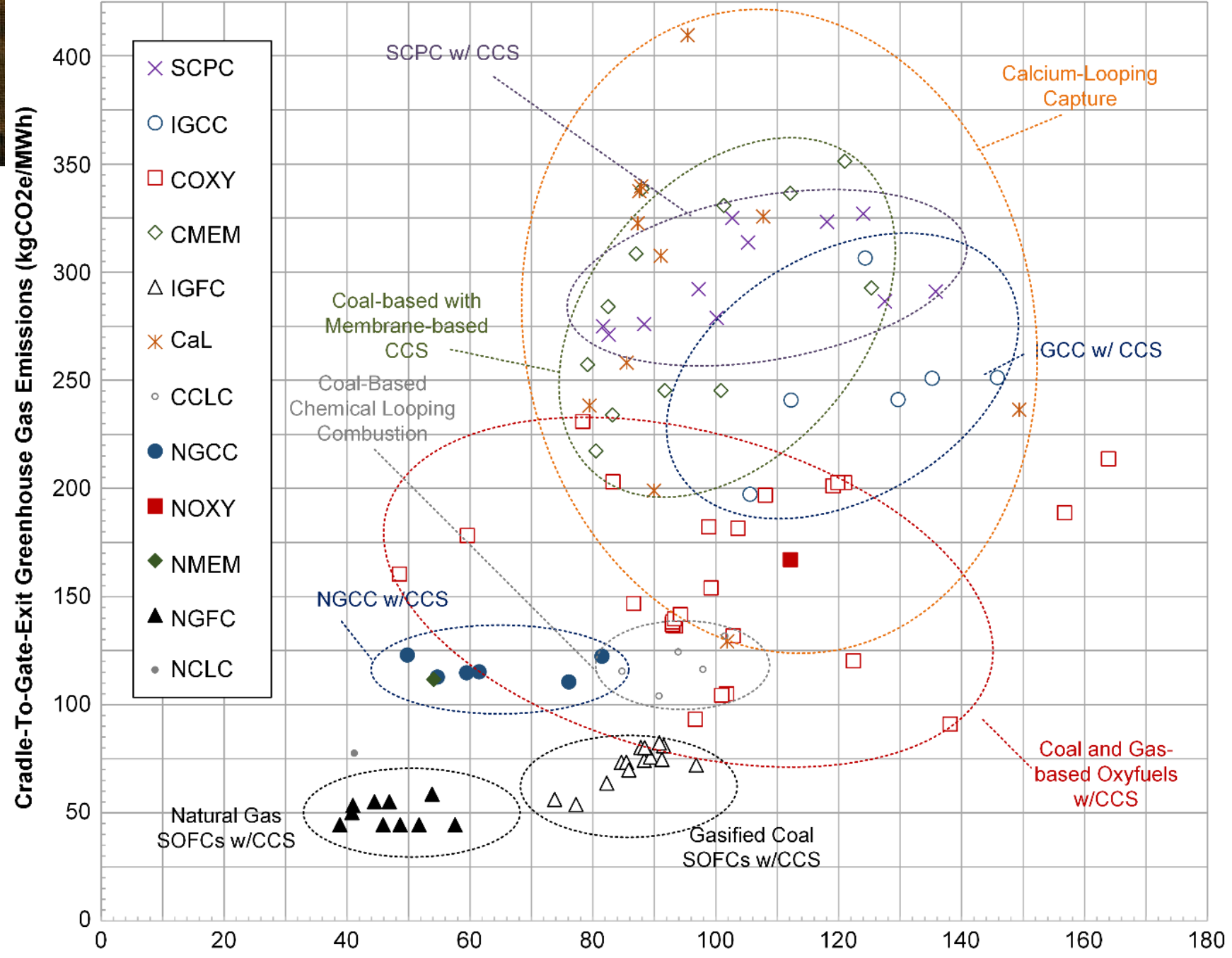
- Solution: Meta-Study of ~100 published data points on those 8 processes.
- Convert to a standard basis of comparison

Standards

- **Size:** 550 MW net, plant gate
 - Nonfuel costs scaled with power law method $p=0.9$
- **Time & Place:** 1Q2016 USA
 - **Time:** North American Plant Cost Index
 - **Place:** Purchasing Power Parity Index
- **Fuel**
 - US Bituminous Coal #6 2016 Avg Price
 - US Conventional Average Gas Mix 2016 Avg Price
- **Captured CO₂ at plant gate**
 - **Pressure:** >115 bar
 - **Purity:** >95 mol%
 - **Capture Rate:** 90-100%
- **LCA:** Cradle to Gate GHG
 - Consistent NO_x production where neglected in original
 - Standardize cradle-to-plant-entrance life cycle impacts
- **CCA:** Cost of CO₂ Avoided
 - Same standard plant without CCS
 - SCPC and NGCC US baseline std's

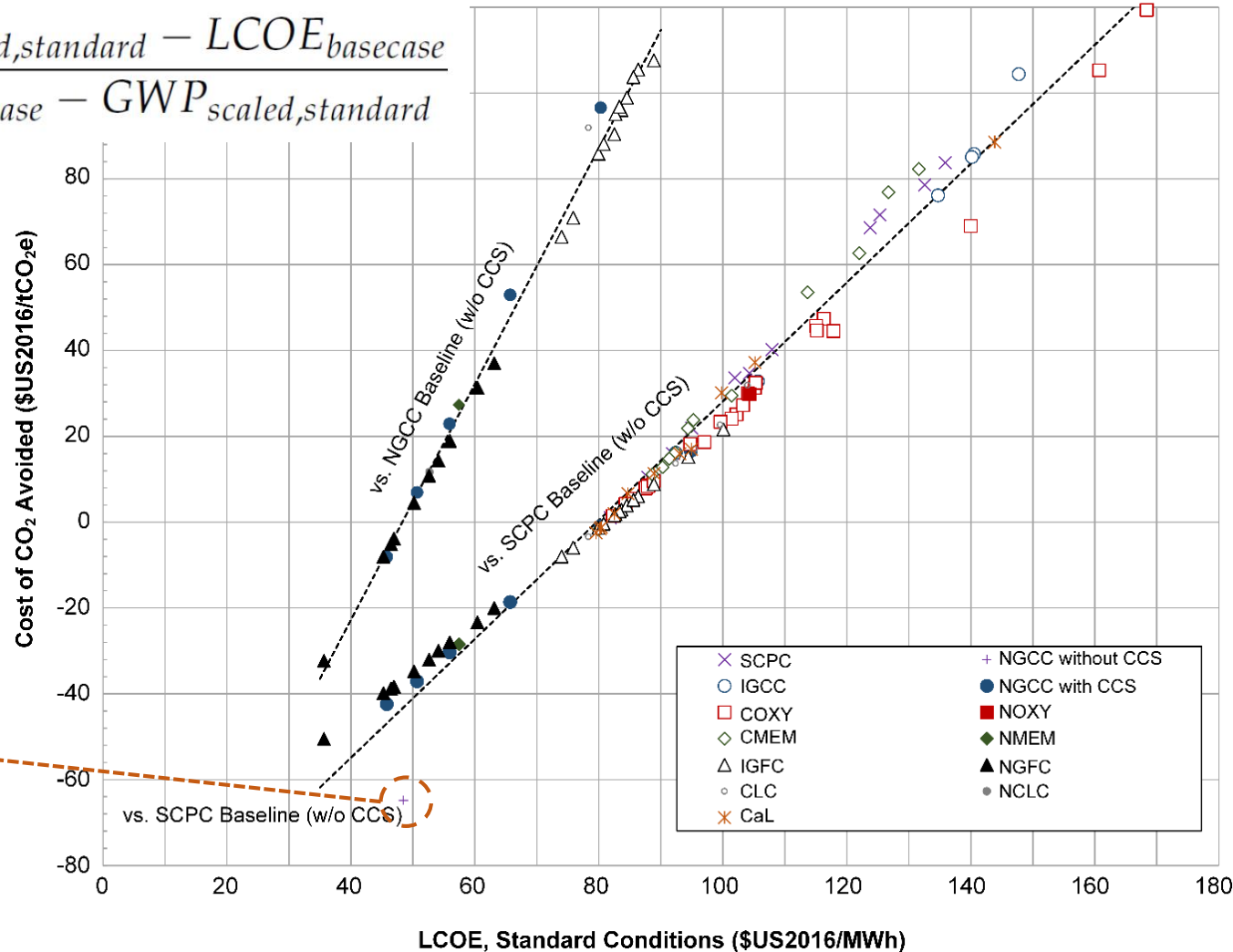
Overall

- SOFC clear winner for coal and gas
- NGCC w/CCS excellent near term solution
- No point in using membranes!
- Oxyfuels / CLC good coal intermediate step



Cost of CO₂ Avoided

$$CCA = \frac{LCOE_{scaled,standard} - LCOE_{basecase}}{GWP_{basecase} - GWP_{scaled,standard}}$$

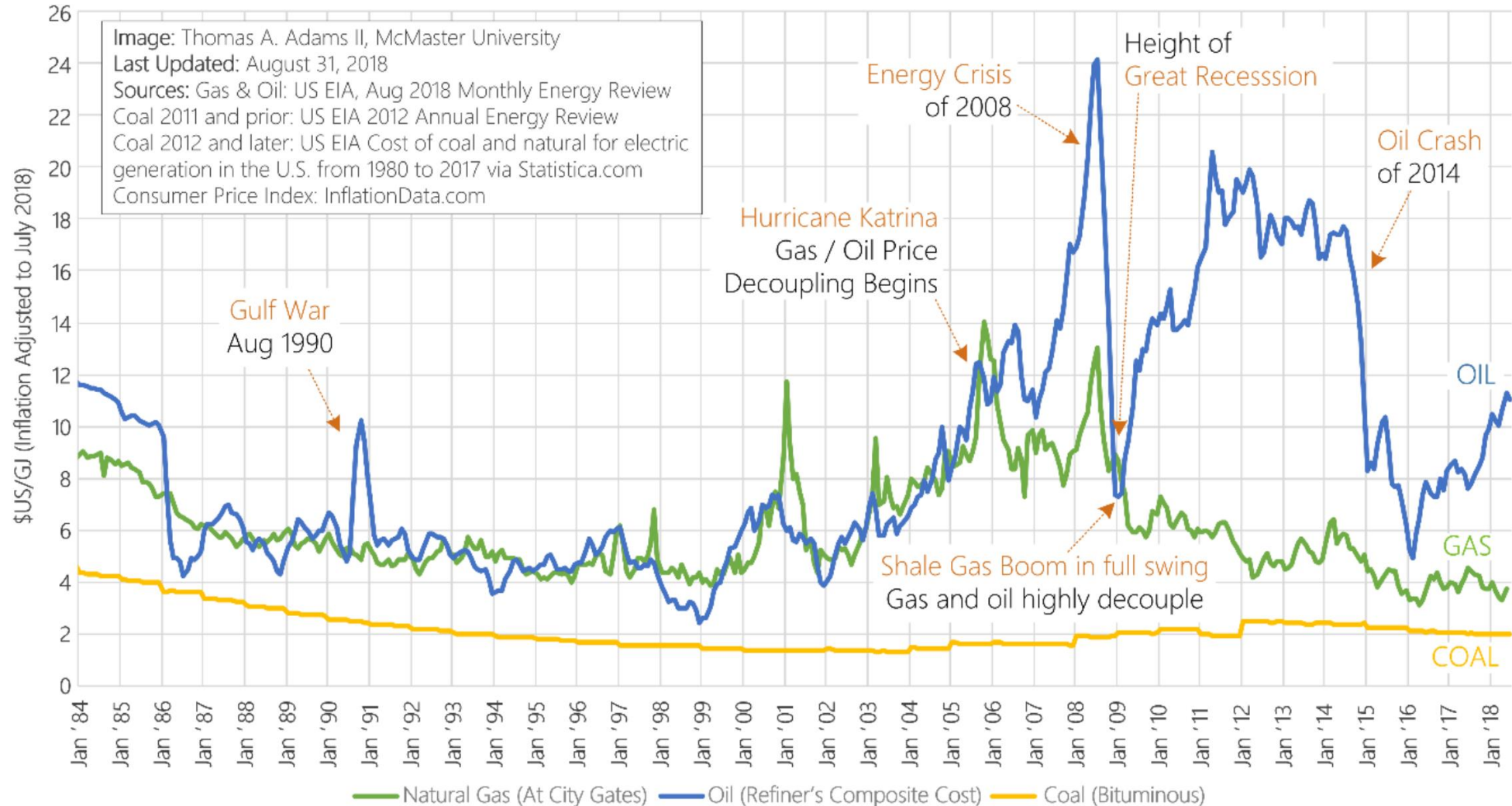


Special Point:
Switching from coal to gas w/o CCS
No point to new coal at all in North America!

Sweet Spot:
The best of post-combustion solvent systems are the only mature technology to be competitive.
Rest requires CO₂/H₂O style power gen.

Negative CCA means:
Gas is so cheap in North America, there is no point to using coal at all.

Price Trends



Meta-Study Conclusions

- **No point to building new coal**
 - (as long as gas prices stay low)
 - IGCC cannot compete with SCPC
 - Calcium Looping unlikely to either

- **Membranes not so promising**
 - **Coal:** Only fictional membranes could compete with solvents at the system level
 - **Gas:** At best competes with solvent directly, maturity / lifetime issues aside.

- **SOFC is best way to use coal**
 - (Could be better than gas in Asian context. Asian study needed!)

FINAL RECOMMENDATIONS

- **Near Term:** Use NGCC with CCS
 - Closest thing we have to commercial
- **Long Term:** Use SOFCs with CCS
 - Needs research and investment now
 - Best fossil fuel approach possible
 - Translates well in foreign situations

Expanding and Standardizing

Big Picture Lessons from Study

- Rather hard to do cross-comparative research of eco-techno-economic analyses (ETEAs)
- But the rewards of doing meta-studies like this are significant
- A standardization of ETEA methodology for the field would greatly amplify the impact of each of our own studies

~O(1,000-10,000) researcher-hours

Very useful society, business, and policy conclusions

Individual studies would have greater influence

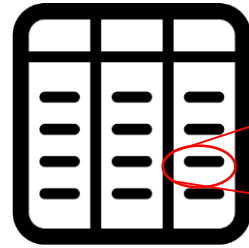
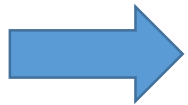
Proposal: Develop recognized standards for performing TEAs and ETEAs

Standard Types	Details...
Base Case Status Quo For Comparison	“Standard” power plants, “standard” refineries, “standard” chemical processes, etc.
Life Cycle Analysis Methodologies	Existing ISO standards, boundary definitions, impact analyses assumptions, methods, etc.
Plant Sizing / Delivered Products	Standard representative capacities and qualities
Metric Definitions	CCA, NPV, efficiencies, HHV vs LHV, other assumptions
Cost Estimations	Standard cost curves, approaches, and assumptions
Transparency and Verifiability	Spreadsheets and models released open-access
Data Formats	Open document formats, etc.

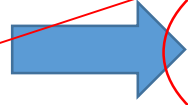
Example Use of Standards: Authors



Researcher
Defines ETEA
Study **as Usual**



Consults
**standards
table**



PSE-3:
*Fuels,
North America,
Large Scale*

**Selects appropriate,
scenario, assumptions
and metrics**

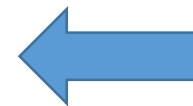


**Research
Performed**



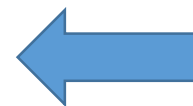
$NPV_{PSE-3} = \$1.2$ bln
 $CCA_{PSE-3} = \$40.3$ /tonne
 $GHG_{PSE-3} = 4.5$ tCO₂e

**Metrics Computed
according to
Standard**



$NPV_{alternate} = \$1.3$ bln
 $CCA_{alternate} = \$41.3$ /tonne
 $GHG_{alternate} = 4.2$ tCO₂e

**Non-standard metrics
also reported (special
cases, etc.)**



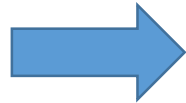
LAPSE
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1000 @article{Klein_2019, author = {Klein, Thomas}, title = {Semicontinuous Thermal Separation Systems}, journal = {Energy}, year = {2019}, volume = {174}, pages = {1150-1162}, doi = {10.1016/j.energy.2018.12.085}, url = {https://doi.org/10.1016/j.energy.2018.12.085}, keywords = {Thermal separation; Semicontinuous; Energy efficiency; Process optimization}, abstract = {This paper presents a novel thermal separation process for the separation of a mixture of two components. The process is designed to be semicontinuous, allowing for a significant reduction in energy consumption compared to traditional batch processes. The process is modeled using Aspen Plus and the results are compared to those of a traditional batch process. The results show that the semicontinuous process can achieve a 30% reduction in energy consumption while maintaining the same separation efficiency. The process is also shown to be more flexible and easier to scale up than traditional batch processes. The paper concludes that the semicontinuous process is a promising alternative to traditional batch processes for the separation of mixtures of two components.}
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**Paper Published. Models /
spreadsheets / code **released**
to public database**

Example Use of Standards: Readers



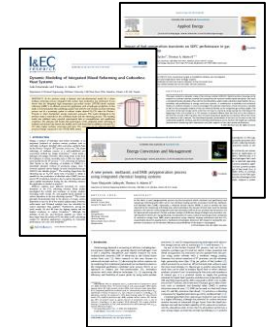
$$NPV_{PSE-3} = \$1.2 \text{ bln}$$

$$CCA_{PSE-3} = \$40.3/\text{tonne}$$

$$GHG_{PSE-3} = 4.5 \text{ tCO}_2\text{e}$$



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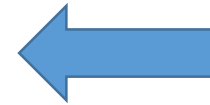
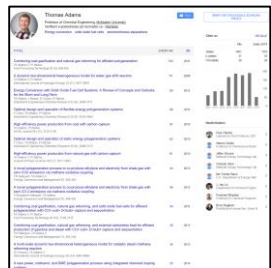


Reader studies paper using PSE standard

Reader sees standard metrics, immediately understood

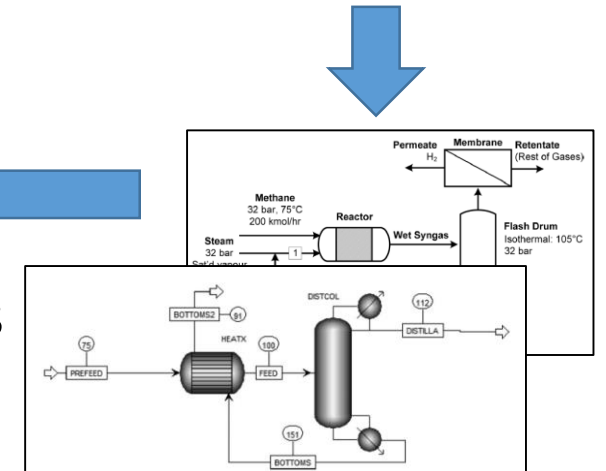
Reader downloads files and data to verify results

Reader considers other papers using the same standards



Reader rapidly performs comparisons and research

Reader easily incorporates standardized models into own work



All standardized research has high impact and citations!

Standardization Committee

- Call for members and stakeholder input
- Go to <http://PSEcommunity.org/standards>

PSE Community.org
The World Community for Chemical Process Systems Engineering Education and Research

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Standards for Techno-Economic Analyses and Eco-Techno-Economic Analyses

PSEcommunity.org supports the development of a uniform set of standards that are used when conducting Techno-Economic Analyses (TEAs) and Eco-Techno-Economic Analyses (ETEAs) on chemical and energy process systems. The standards would provide a uniform basis for comparing one process design concept to another across literature studies. This is currently almost impossible to do because each individual research study uses its own methods, assumptions, and definitions when performing analyses of proposed process concepts. However, each research study that conducted its TEA or ETEA adhering to this standard could be directly compared to another other, using established procedures, with little effort.

[Example Use of Standards: Authors](#)

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Wrap Up

- We can learn a lot from **eco-techno-economic meta studies**
 - Critical for **taking meaningful and near-term action** on climate change
 - Critical for **policy** and **business**
 - **See through the hype.**
- Current **culture of the field:**
 - Hide models and code
 - C.Y.A.
 - Nonstandard methods
 - Not working toward common goal
- **Goal:** Make it **as easy as possible** for others to use and understand your research for societal benefit
 - **Join me!**